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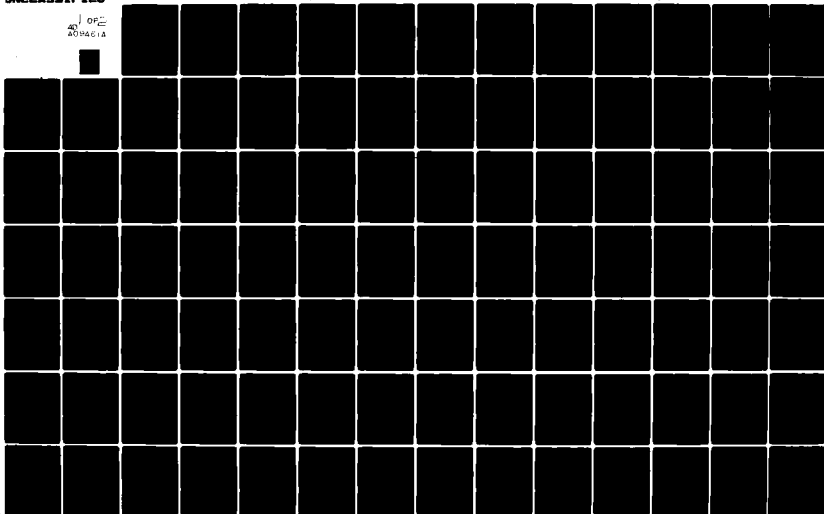
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NUMERICAL SOLUTION OF STEADY AND PERIODICALLY PULSED TWO-DIMENS--ETC(U)  
APR 80 J C LAI, J M SIMMONS

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20 PAGES



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Numerical Solution of Steady and  
Periodically Pulsed Two-Dimensional  
Turbulent Free Jets,

by

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Joseph C. S. Lai

and

J. M. Simmons

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April 1980

Approved for public release; distribution  
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Prepared for  
Naval Air Systems Command  
Washington, D.C. 20361

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SECURITY CLASSIFICATION OF THIS PAGE (When Data Entered)

REPORT DOCUMENTATION PAGE		READ INSTRUCTIONS BEFORE COMPLETING FORM
1. REPORT NUMBER NPS67-80-015	2. GOVT ACCESSION NO. AD-A094 614	3. RECIPIENT'S CATALOG NUMBER
4. TITLE (and Subtitle) Numerical Solution of Steady And Periodically Pulsed Two-Dimensional Turbulent Free Jets		5. TYPE OF REPORT & PERIOD COVERED Technical Report
		6. PERFORMING ORG. REPORT NUMBER
7. AUTHOR(s) Joseph C. S. Lai and J. M. Simmons		8. CONTRACT OR GRANT NUMBER(s)
9. PERFORMING ORGANIZATION NAME AND ADDRESS NAVAL POSTGRADUATE SCHOOL Monterey, CA 93940		10. PROGRAM ELEMENT, PROJECT, TASK AREA & WORK UNIT NUMBERS 61153N N00019-80-WR-01199
11. CONTROLLING OFFICE NAME AND ADDRESS NAVAL POSTGRADUATE SCHOOL Monterey, CA 93940		12. REPORT DATE April 1980
		13. NUMBER OF PAGES 110
14. MONITORING AGENCY NAME & ADDRESS (if different from Controlling Office) NAVAL POSTGRADUATE SCHOOL Monterey, CA 93940		15. SECURITY CLASS. (of this report)
		15a. DECLASSIFICATION/DOWNGRADING SCHEDULE
16. DISTRIBUTION STATEMENT (of this Report)  Approved for public release, distribution unlimited		
17. DISTRIBUTION STATEMENT (of the abstract entered in Block 20, if different from Report)		
18. SUPPLEMENTARY NOTES		
19. KEY WORDS (Continue on reverse side if necessary and identify by block number) turbulent jets, viscous/inviscid interactions, shear flows, turbulence modelling, computational fluid dynamics, Cebeci-Keller box method		
20. ABSTRACT (Continue on reverse side if necessary and identify by block number) The flow fields of a steady and a periodically pulsed two-dimensional turbulent free jet have been studied by solving the thin shear layer equations by the Keller Box method in transformed variable form. A constant eddy-viscosity formulation was used to model the Reynolds shear stress term. For the steady jet, calculations agree well with documented experimental data. Computed results of the unsteady jet indicate that the mean flow characteristics follow closely those of the steady jet and compare well with		

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## TABLE OF CONTENTS

	PAGE
Abstract . . . . .	v
Acknowledgement . . . . .	vi
Nomenclature . . . . .	vii
1.0 Introduction . . . . .	1
2.0 Governing Equations . . . . .	4
2.1 Governing Equations in Non-dimensional Form . . . . .	7
2.2 Turbulence Modelling . . . . .	8
2.3 Governing Equations in Transformed Variable Form . . . . .	12
3.0 Method of Solution . . . . .	14
3.1 Finite Difference Form of the Governing Equations . . . . .	15
3.2 Time-Varying Velocity Profile at the Nozzle Exit . . . . .	19
3.3 Solution of the Finite Difference Equation . . . . .	22
3.4 Convergence Criterion . . . . .	24
3.5 Criterion for the Spreading of Jet . . . . .	25
3.6 Criterion for the Attainment of Steady State Solution . . . . .	27
3.7 Mean Momentum Flux, Phase Angle and Peak to Peak Oscillation . . . . .	29
3.7.1 Mean Momentum Flux . . . . .	29
3.7.2 Phase Angle . . . . .	29
3.7.3 Peak to Peak Oscillation . . . . .	30

	PAGE
4.0 Results and Discussions . . . . .	32
4.1 Steady Jet . . . . .	33
4.2 Unsteady Jet . . . . .	37
4.2.1 Sensitivity of the Solution to the Convergence Criterion . . . .	37
4.2.2 Validity of the Criterion for the Attainment of Steady State Solution . . . . .	38
4.2.3 Sensitivity of the Solution to Time Step . . . . .	38
4.2.4 Relaxation of the Criterion for Jet Spreading . . . . .	38
4.2.5 Results . . . . .	39
5.0 Concluding Remarks . . . . .	43
6.0 References . . . . .	45
Appendix A Structure and Listing of Computer Program . . . . .	48
Appendix B Figures . . . . .	79
Initial Distribution List . . . . .	80

# ABSTRACT

The flow fields of a steady and a periodically pulsed two-dimensional turbulent free jet have been studied by solving the thin shear layer equations by the Keller Box method in transformed variable form. A constant eddy-viscosity formulation was used to model the Reynolds shear stress term. For the steady jet, calculations agree well with documented experimental data. Computed results of the unsteady jet indicate that the mean flow characteristics follow closely those of the steady jet and compare well with available experimental data. For sufficiently high frequency and amplitude of pulsation or at large streamwise distance, significant unsteady effects occur in the instantaneous quantities.



## ACKNOWLEDGEMENT

This work was supported by the Australian Research Grants Committee under Reference No. F77/15026 and by the Naval Air Systems Command, Code AIR 310 under contract No. N0001980WR01199, Job Order No. 57763 Segment 1385/4. The first author (JCSL) is grateful to Professor M. F. Platzer for his encouragement and support during his 6-months visit at the Naval Postgraduate School. Also, thanks are extended to Professor T. Cebeci for his valuable comments.

## NOMENCLATURE

Unless otherwise stated, the symbols used in the text have the following meanings.

a	constant defined in Eq. (15a)
b	constant defined in Eq. (15b)
c	constant defined in Eq. (11)
F	% peak-to-peak oscillation of centre-line velocity
f	stream function in $(\zeta, t, \eta)$ coordinates defined in Eq. (15b)
h	nozzle width
M	mean momentum flux in streamwise direction
$p^*$	mean pressure
$p^*$	instantaneous pressure
Q	mean mass flow at any streamwise station
$Q_E$	mean mass flow at nozzle exit
T	period of pulsation
t	non-dimensional time = $U_{ci}^* t^* / h$
U	non-dimensional mean x-component velocity = $U^* / U_{ci}^*$
$U_o(y)$	non-dimensional mean velocity profile at the nozzle exit
u	non-dimensional instantaneous x-component velocity = $u^* / U_{ci}^*$
$u'$	non-dimensional x-component velocity fluctuation = $u'^* / U_{ci}^*$
V	non-dimensional mean y-component velocity = $V^* / U_{ci}^*$
v	non-dimensional instantaneous y-component velocity = $v^* / U_{ci}^*$

$v'$	non-dimensional y-component velocity fluctuation = $v^{*}/U_{ci}^{*}$
$x$	non-dimensional streamwise distance - $x^{*}/h$
$y$	non-dimensional transverse distance - $y^{*}/h$
$y_{\frac{1}{2}}$	value of $y$ at which $U = \frac{1}{2}U_c$

#### GREEK SYMBOLS

$\Delta$	difference between two quantities
$\epsilon$	amplitude of pulsation
$\nu$	non-dimensional kinematic viscosity = $\nu^{*}/(U_{ci}^{*}h)$
$\nu_t$	eddy-viscosity defined in Eq. (10)
$\nu_{eff}$	Effective eddy viscosity defined in Eq. (13)
$\psi$	stream function in $(\zeta, t, y)$ coordinates defined in Eq. (15b)
$\phi$	phase angle
$\Phi$	function defined in Eq. (28)
$\eta$	transformed variable defined in Eq. (15b)
$\omega$	non-dimensional angular frequency of pulsation = $\omega^{*}h/U_{ci}^{*}$
$\zeta$	non-dimensional distance identical to $x$
$\zeta_0$	constant defined in Eq. (15a)

#### SUPERSCRIPT

$*$	dimensional quantities
-----	------------------------

# SUBSCRIPTS

c	centerline
i	initial
$\infty$	jet edge
Overbar	time-average quantities

## 1.0 Introduction

The steady two-dimensional turbulent jet has long been the subject of many theoretical and experimental investigations because of its important role in many different types of engineering applications such as fluidic and combustion systems and because of its significance in providing fundamental understanding to the physics of flow mechanisms such as turbulence and vortex structures. Owing to its simplicity in configuration, the steady two-dimensional turbulent jet has been studied in detail experimentally and is regarded as one of the most well-documented flows in the literature where sufficient data are available for many practical engineering purposes. However, despite such extensive investigations, for example Heskestad (1965), Gutmark and Wygnanski (1976) and Everitt and Robins (1978), considerable scatter is found to exist between the results of various workers even in the mean flow parameters such as centre-line velocity decay rate and jet spreading rate. Such discrepancies have been casually attributed to different effects such as Reynolds number, aspect ratio, nozzle geometry, initial conditions, upstream turbulence intensities and the uncertainties involved in the hot wire results in regions where reversed flow may occur. Nevertheless, no unified agreement on the effects of such factors and other flow mechanisms on the flow development has been reached. A

comprehensive review and evaluation of the experiemntal data on steady turbulent jets was given by Harsha (1971) and Rodi (1975).

The analytical solution of the fully-developed steady turbulent jet was first sought by Tollmien (1926) followed by Goertler (1942) and Schlichting (1965). With the advent of computer technology and the rapid development of numerical techniques, the steady turbulent jets have commonly been used for turbulence modelling and as standard test cases of turbulence models. Many numerical predictions of steady turbulent jets using various turbulence models have been attempted such as Rodi and Spalding (1970), Launder et al (1972) and Chen and Nikitopoulos (1979) to calculate the flow properties and to complement the experimental results.

Although almost inevitably unsteadiness of varying degrees occurs in practice either desirably to achieve certain favorable characteristics or undersirably due to the fluctuations in the surrounding fluid, very few results appear to have been reported on unsteady turbulent jets both theoretically and experimentally. Only until recently, because of the growing realization of the fundamental and practical implications of an improved understanding of unsteady effects, the excitation of turbulent jets by acoustic (Fiedler and Korschelt (1979)), mechanical (Bremhorst and Harch (1979)) and fluidic (Piatt and Viets (1979)) means has received considerable attention. On the other hand,

closed form solutions of the unsteady jets which adequately describe the flow development can hardly be obtained despite the efforts of Pai (1965) and McCormack et al (1966).

Numerical solution of unsteady laminar jets was obtained by Kent (1973). Although turbulence models have been developed to give sufficiently accurate predictions of a wide variety of steady flows, the applicability of such turbulence models to unsteady flows is uncertain.

The objectives of this study are to apply the transformation developed by Lai and Simmons (1978) to compute steady and unsteady turbulent jets, to add to the understanding of the steady and unsteady two-dimensional turbulent free jets, to investigate the validity of quasi-steady approximations and to evaluate the suitability of using turbulence models established for steady flows in unsteady flow calculations. The unsteady jet considered consists of an initially steady, two-dimensional, turbulent free jet with a sinusoidal mass flow variation superimposed on it at the nozzle exit. The steady-state oscillatory flow characteristics at any location downstream of the nozzle are obtained by solving the thin shear layer equations in two spatial ( $\zeta, \eta$ ) and one time ( $t$ ) transformed coordinates.

## 2.0 Governing Equations

The Navier-Stokes equations for two-dimensional incompressible flow in tensor notations are given by (see, e.g., Hinze (1975))

$$\frac{\partial U_i^*}{\partial t^*} + u_j^* \frac{\partial U_i^*}{\partial x_j^*} = - \frac{1}{\rho} \frac{\partial p^*}{\partial x_i^*} + \nu^* \frac{\partial^2 U_i^*}{\partial x_j^* \partial x_j^*} \quad (1)$$

with the continuity equation being given by

$$\frac{\partial u_i^*}{\partial x_i^*} = 0 \quad (2)$$

By applying Reynolds decomposition

$$u_i^* = U_i^* + u_i^{*'} , \text{ etc.}$$

to equation (1) and taking time average with a time scale large compared with that of the turbulent motions but small compared with the periodicity of the flow, the time-averaged Reynolds equations can then be given by

$$\begin{aligned} \frac{\partial U_i^*}{\partial t^*} + U_j^* \frac{\partial U_i^*}{\partial x_j^*} = & \frac{1}{\rho} \frac{\partial}{\partial x_j^*} (-P^* + \frac{\partial U_i^*}{\partial x_j^*} + \frac{\partial U_j^*}{\partial x_i^*} \\ & - \overline{\rho u_i^{*'} u_j^{*'}} \end{aligned} \quad (3)$$

Consider an unsteady, two-dimensional, constant property, turbulent free jet issuing into a stationary medium. The instantaneous configuration is shown schematically in Fig. 1.



Assuming the thin shear layer approximations as in Cebeci and Bradshaw (1977), the governing equations can be obtained from equations (2) and (3) to yield in rectangular coordinate system

$$\frac{\partial U^*}{\partial x^*} + \frac{\partial V^*}{\partial y^*} = 0 \quad (4a)$$

$$\text{and} \quad \frac{\partial U^*}{\partial t^*} + U^* \frac{\partial U^*}{\partial x^*} + V^* \frac{\partial U^*}{\partial y^*} = \frac{\partial}{\partial y^*} (v^* \frac{\partial U^*}{\partial y^*} - \overline{u^{*'} v^{*'}}) \quad (4b)$$

The boundary conditions on the centre-line and at the edge of the jet can be expressed respectively by

$$t^* \geq 0 \quad \begin{cases} y^* = 0 & \frac{\partial U^*}{\partial y^*} = V^* = 0 \\ y^* = y_\infty & U^* = 0 \end{cases} \quad (5a)$$

$$(5b)$$

The time-varying boundary condition at the nozzle exit is given by

$$t^* \geq 0 \quad x^* = 0 \quad U^* = U_0^*(y^*) (1 + \epsilon \sin \omega^* t^*) \quad (6a)$$

where  $U_0^*(y^*)$  is the mean velocity profile at the nozzle exit,  $\epsilon$  is the amplitude of pulsation and  $\omega^*$  is the angular frequency of pulsation.

For all locations downstream of the nozzle, the initial conditions are given by

$$t^* = 0 \quad x^* \geq 0 \quad U^* = U_i^*(x^*, y^*) \quad (6b)$$

where  $U_i^*(x^*, y^*)$  is the steady state solution of equation (4) with the boundary condition at the nozzle exit given by equation (6a) with  $t^* = 0$ .

## 2.1 Governing Equations in Non-Dimensional Form:

In order to enable the solution obtained to be valid for a family of velocity profiles which have the same normalized shape at the nozzle exit, the following non-dimensional variables are used: -

$$U(x,y,t) = \frac{U^*(x^*,y^*,t^*)}{U_{ci}^*}, \quad V(x,y,t) = \frac{V^*(x^*,y^*,t^*)}{U_{ci}^*}$$

$$x = \frac{x^*}{h} \quad y = \frac{y^*}{h} \quad t = \frac{U_{ci}^*}{h} t^* \quad \omega = \frac{h}{U_{ci}^*} \omega^*$$

$$v = \frac{v^*}{U_{ci}^* h} \quad \overline{u'v'} = \frac{\overline{u'^* v'^*}}{U_{ci}^{*2}}$$

where  $U_{ci}^*$  is the centre-line velocity at the nozzle exit at  $t^* = 0$ .

Equation (4) can now be written as

$$\frac{\partial U}{\partial x} + \frac{\partial V}{\partial y} = 0 \quad (7a)$$

$$\frac{\partial U}{\partial t} + U \frac{\partial U}{\partial x} + V \frac{\partial U}{\partial y} = \frac{\partial}{\partial y} \left( v \frac{\partial U}{\partial y} - \overline{u'v'} \right) \quad (7b)$$

subject to the following boundary and initial conditions

$$t \geq 0 \quad \begin{cases} y = 0 & \frac{\partial U}{\partial y} = V = 0 \\ y = \infty & U = 0 \end{cases} \quad (8a)$$

$$(8b)$$

$$t \geq 0 \quad x = 0 \quad U = U_0(y) (1 + \epsilon \sin \omega t) \quad (9a)$$

$$t = 0 \quad x \geq 0 \quad U = U_i(x,y) \quad (9b)$$

## 2.2 Turbulence Modelling

The Navier-Stokes equations constitute a complete set of equations of motion which can in theory be solved to yield a solution for any laminar or turbulent flow field. However, turbulence comprises a wide range of length scales bounded from above by the dimensions of the flow field and bounded from below by the diffusive action of molecular viscosity. The resolution scale of the smaller eddies which are responsible for the decay of turbulence is too small that it precludes the use of any existing computer. Furthermore, very often only the time-averaged properties are of interest in engineering applications even if the flow is time dependent. Hence, the Navier-Stokes equations are time-averaged first before being solved. This avoids not only the difficulty in representing all the characteristic turbulence scales but also unnecessary computations of transients if only the time-averaged properties are required. The process of time-averaging such as the Reynolds time-averaging described in section 2.0 causes the loss of certain information contained in the original equations and results in more unknowns than the governing equations through the introduction of statistical correlations of fluctuating velocities such as the  $\overline{u'v'}$  term in equation (7b) which are known as apparent Reynolds stresses and are responsible for the actual momentum

transfer. Attempts to derive additional equations for those Reynolds stresses will only result in additional unknowns. Thus the time-averaging process presents a closure problem which is to reduce the number of unknowns to equal the number of governing equations. In order to achieve this, the additional unknown quantities must be modelled or approximated in terms of known quantities through a set of equations which, when solved with the mean-flow equations, simulate the actual flow situation. This process is generally termed "turbulence modelling."

Turbulence models can broadly be classified into "first-order" models in which the mean flow equations are solved without additional partial differential equations for the velocity fluctuation terms and "higher-order" models in which transport equations for higher-order velocity correlations are solved with the mean flow equations. Since in the "first-order" models additional partial differential equations are not solved for the turbulence quantities which are expressed in terms of known quantities through certain algebraic formulation, they are known as zero-equation models and "higher-order" models which involve at least one partial differential equation for the turbulence quantities can thus be termed one-equation or two-equation models, etc. A description of the various types of turbulence models can be found in Launder and Spalding (1972) and a comprehensive review of the state-of-art is given by Reynolds and Cebeci (1978).

Zero-equation models which are based on empirical correlations of the extensive available experimental data and mostly on the eddy-viscosity and mixing-length concepts such as the Cebeci-Smith eddy viscosity model (1974) have been widely used and proved to be very successful in obtaining very accurate predictions of non-separating flows. For more complex flows which involve recirculation and separation, the more refined two-equation  $k-\epsilon$  model described by Launder and Spalding (1976) is the most well-developed among all other "high-order" models. It has been recognized that although "higher-order" models contain more information and hence simulate the flow situation more realistically than the "first-order" models, they are more difficult to solve and require generally an order-of-magnitude more computing storage and time while in non-separating and simple flow situations, the first-order models can yield predictions to the same degree of accuracy as the "higher-order" models. It is in the light of this philosophy that in this study, a constant-eddy viscosity model due to Prandtl (1942) is used.

By employing the eddy-viscosity concept of Boussinesq, the fluctuating-velocity correlation term  $\overline{u'v'}$  in equation (7b) is related to the mean velocity gradient through the eddy viscosity  $\nu_t$  as follows:

$$\overline{u'v'} = -\nu_t \frac{\partial U}{\partial y} \quad (10)$$

The eddy viscosity  $\nu_t$  can then be obtained from the constant eddy-viscosity model as

$$\nu_t(t) = c y_{1/2} U_c(t) \quad (11)$$

where  $c$  is a constant, and  $y_{1/2}$  is the jet half-width.

In this model, two constants  $c_1$  and  $c_2$  are used for the free jet as it emerges from developing to fully developed form. Hence  $c$  is given by

$$c = \begin{cases} c_1 & \text{if } \bar{U}_c \geq 0.95 \\ c_2 & \text{if } \bar{U}_c < 0.95 \end{cases} \quad (12)$$

By defining an effective eddy viscosity  $\nu_{eff}$  such that

$$\nu_{eff} = \nu_t + \nu \quad (13)$$

and using equation (10), equation (7b) can then be written as

$$\frac{\partial U}{\partial t} + U \frac{\partial U}{\partial x} + V \frac{\partial U}{\partial y} = \frac{\partial}{\partial y} (\nu_{eff} \frac{\partial U}{\partial y}) \quad (14)$$

Hence the flow development of a periodically pulsed turbulent free jet is governed by equations (7a) and (14) subject to the boundary and initial conditions of equations (8) and (9) with the constant eddy viscosity model of (11)

### 2.3 Governing Equation in Transformed Variable Form

It has been shown by Lai and Simmons (1978) that transformations based on the similarity solutions are successful in reducing substantially the rate of spread of an unsteady laminar jet, hence enabling the use of variable grid sizes over predetermined regions. In this study, similar transformations are employed. A dimensionless transverse distance  $\eta$  and a dimensionless stream function  $\psi$  are defined by

$$\eta = ay/(\zeta + \zeta_0) \quad (15a)$$

$$\psi(\zeta, y, t) = b(\zeta + \zeta_0)^{1/2} f(\zeta, \eta, t) \quad (15b)$$

where  $a$ ,  $b$  and  $\zeta_0$  are arbitrary constants which can be varied to facilitate computation and  $x$  is renamed as  $\zeta$ .

The function  $f$  automatically satisfies the continuity equation (7a) and equation (14) can be re-written in the transformed coordinates as

$$\begin{aligned} (\zeta + \zeta_0)^{-1/2} [v_{eff} f'']' + (f')^2 + ff'' = 2(\zeta + \zeta_0) [f' \frac{\partial f'}{\partial \zeta} \\ - f'' \frac{\partial f}{\partial \zeta} + \frac{(\zeta + \zeta_0)^{1/2}}{ab} \frac{\partial f'}{\partial t}] \end{aligned} \quad (16)$$



where prime denotes differentiation with respect to  $\eta$ ,

$$f' = (\zeta + \zeta_0)^{1/2} U/ab \quad (17)$$

and  $a$  and  $b$  are chosen for convenience such that  $a/b = \frac{1}{2}$ .

The boundary conditions in equation (8) become

$$t > 0 \quad \begin{cases} \eta = 0 & f'' = 0 & f + 2(\zeta + \zeta_0) \frac{\partial f}{\partial \zeta} = 0 \\ \eta = \eta_\infty & f' = 0 \end{cases} \quad (18a)$$

$$(18b)$$

The initial conditions at  $\zeta = 0$  in the  $(\eta, t)$  plane is obtained by writing equation (9a) with equation (17) as

$$f' = f'_0(\eta)(1 + e \sin \omega t) \quad (19a)$$

The initial conditions at  $t = 0$  in the  $(\zeta, \eta)$  plane are generated by the solutions  $U_1(\zeta, \eta)$  of the following steady jet equation obtained from equation (16)

$$(\zeta + \zeta_0)^{-1/2} [v_{eff} f'']' + (f')^2 + ff'' = 2(\zeta + \zeta_0) [f' \frac{\partial f'}{\partial \zeta} - f'' \frac{\partial f}{\partial \zeta}] \quad (19b)$$

The effective eddy-viscosity can be obtained from equation (13) using equations (11) and (15) to give

$$v_{eff}(t) = cb(\zeta + \zeta_0)^{1/2} \eta_{1/2} f'_c(t) + v \quad (20)$$

where  $c$  is subject to the conditions specified in equation (12).

### 3.0 Method of Solution

Since the initial conditions in the  $(\zeta, \eta)$  plane are generated by solving the steady jet equation (19b) subject to the boundary conditions in equation (18), the flow development of the steady jet is first studied. For computer programme development purpose, two separate computer programs were written for the steady and unsteady jet respectively with the solutions of the steady jet stored on disk for use in the unsteady jet program. However, if necessary, the steady jet program can easily be incorporated into the unsteady one. Both equations (16) and (19b) are parabolic and can be solved by a marching procedure. The finite difference scheme employed is the Box Method developed by Keller (1970), and described in detail by Cebeci and Bradshaw (1977). The scheme has been applied successfully to a wide range of boundary-layer type of flows including both time-dependent and separating flows by Cebeci and his co-workers (e.g., see Bradshaw et al (1980)).

### 3.1 Finite Difference Form of the Governing Equations

Equation (16) is rewritten as a system of first order partial differential equations -

$$f' = g \quad (21a)$$

$$g' = q \quad (21b)$$

$$\begin{aligned} (\zeta + \zeta_0)^{-1/2} [v_{\text{eff}} q]' + g^2 + fq = 2(\zeta + \zeta_0) \left[ g \frac{\partial g}{\partial \zeta} - q \frac{\zeta f}{\partial \zeta} \right. \\ \left. + \left( \frac{\zeta + \zeta_0}{ab} \right)^{1/2} \frac{\partial g}{\partial t} \right] \end{aligned} \quad (21c)$$

Consider the net cube shown in Fig. 2 and denote the grid points by

$$\zeta_0 = 0 \quad \zeta_{i+1} = \zeta_i + r_i \quad i = 1, 2, \dots, I$$

$$t_0 = 0 \quad t_n = t_{n-1} + k_n \quad n = 1, 2, \dots, N$$

$$\eta_0 = 0 \quad \eta_j = \eta_{j-1} + h_j \quad j = 1, 2, \dots, J$$

$$\eta_J = \eta_\infty$$

where  $i, n, j$  are just sequence numbers and the variable net spacings  $r_i$ ,  $k_n$  and  $h_j$  are completely arbitrary.

In the study of jets, a coarse grid spacing  $h_j$  can be used in the vicinity of the centre line and the edge of the jet as the transverse ( $\eta$ ) gradients of  $f$  are small in those regions. The quantities  $(f, g, q)$  at points  $(\zeta_i, t_n, \eta_j)$  are approximated by the grid functions  $(f_j^{i,n}, g_j^{i,n}, q_j^{i,n})$ . Hence by using central differencing and averaging about the mid-point  $(\zeta_i, t_n, \eta_{j-1/2})$ , Eqs. (21a) and (21b) can be written in the following finite difference forms

$$(f_j^{i,n} - f_{j-1}^{i,n})/h_j = g_{j-\frac{1}{2}}^{i,n} \quad (22a)$$

$$(g_j^{i,n} - g_{j-1}^{i,n})/h_j = q_{j-\frac{1}{2}}^{i,n} \quad (22b)$$

where, for example, the shorthand notation  $g_{j-\frac{1}{2}}^{i,n}$  has been used for  $\frac{1}{2}(g_j^{i,n} + g_{j-1}^{i,n})$

Shorthand notations are introduced, for example,

$$\bar{f}_i = \frac{1}{2}(f_j^{i,n} + f_j^{i,n-1} + f_{j-1}^{i,n} + f_{j-1}^{i,n-1}) = \frac{1}{2}(f_{j-\frac{1}{2}}^{i,n} + f_{j-\frac{1}{2}}^{i,n-1})$$

$$\bar{f}_j = \frac{1}{4}(f_j^{i,n} + f_j^{i-1,n} + f_j^{i,n-1} + f_j^{i-1,n-1}) = \frac{1}{4}(f_j^{i,n} + f_j^{234})$$

$$\bar{f}_n = \frac{1}{4}(f_j^{i,n} + f_j^{i-1,n} + f_{j-1}^{i,n} + f_{j-1}^{i-1,n}) = \frac{1}{2}(f_{j-\frac{1}{2}}^{i,n} + f_{j-\frac{1}{2}}^{i-1,n})$$

$$f_j^{234} = f_j^{i,n-1} + f_j^{i-1,n} + f_j^{i-1,n-1}$$

Eq. (21c) can be approximated using central differencing at  $(\zeta_{i-\frac{1}{2}}, t_{n-\frac{1}{2}}, \eta_{j-\frac{1}{2}})$  by

$$\begin{aligned} (Bq)_j - (Bq)_{j-1} + h_j \{ (g^2)_{j-\frac{1}{2}} + (fq)_{j-\frac{1}{2}} - \alpha [g_{j-\frac{1}{2}}(g_{j-\frac{1}{2}} + \\ g_{j-\frac{1}{2}}^{i,n-1} + g_{j-\frac{1}{2}}^{234} - 2\bar{g}_{i-1}) - q_{j-\frac{1}{2}}(f_{j-\frac{1}{2}} + \\ f_{j-\frac{1}{2}}^{i,n-1} - 2\bar{f}_{i-1}) - f_{j-\frac{1}{2}}q_{j-\frac{1}{2}}^{234}] - \\ \alpha_i g_{j-\frac{1}{2}} \} = \tau_{j-\frac{1}{2}}^{i-1,n-1} \end{aligned} \quad (22c)$$

where  $B = (\zeta + \zeta_0)^{-\frac{1}{2}} v_{eff}$

$$\alpha = \frac{m_1^{i-\frac{1}{2}}}{2r_i}$$

$$m_1 = 2(\zeta + \zeta_0)$$

$$\alpha_1 = \frac{4[(\zeta + \zeta_0)^{3/2}]^{i-\frac{1}{2}}}{ab k_n}$$

$$T_{j-\frac{1}{2}}^{i-1,n-1} = (Bq)_{j-1}^{234} - (Bq)_j^{234} + h_j \{ - (g^2)_{j-\frac{1}{2}}^{234} - (fq)_{j-\frac{1}{2}}^{234} + a[\beta_2 g_{j-\frac{1}{2}}^{234} - \beta_1 q_{j-\frac{1}{2}}^{234}] + \alpha_1 \beta_3 \}$$

$$\beta = g_{j-\frac{1}{2}}^{i,n-1} + g_{j-\frac{1}{2}}^{234} - 2 \bar{g}_{i-1}$$

$$\beta_1 = f_{j-\frac{1}{2}}^{i,n-1} + 2 \bar{f}_{i-1}$$

$$\beta_2 = g_{j-\frac{1}{2}}^{i,n-1} - 2 \bar{g}_{i-1}$$

$$\beta_3 = g_{j-\frac{1}{2}}^{i-1,n} - 2 \bar{g}_{n-1}$$

In the above equation (22c), the superscripts  $i,n$  have been dropped for simplicity.

It has been pointed out by Keller (1978) that in approximating non-linear terms such as  $(fq)_{j-\frac{1}{2}}$  in equation (22c) with the Box scheme, there exists several choices which should not have serious effect on accuracy or stability as long as the proper centering is maintained. However, in jet calculations, it has been found in this study that the approximation of terms such as  $(fq)$  in the form of  $(f)_{j-\frac{1}{2}}(q)_{j-\frac{1}{2}}$

results in better numerical stability at the jet edge.

The boundary conditions in Eq. (18) become

$$q_0^{i,n} = 0 \quad (23a)$$

$$f_0^{i,n} = (1 + \frac{2m_1}{r_i})^{-1} (\frac{2m_1}{r_i} - 1) f_0^{i-1,n} \quad (23b)$$

$$g_J^{i,n} = 0 \quad (23c)$$

The initial conditions at  $\zeta = 0$  in the  $(\eta, t)$  plane in Eq (19a) are given by

$$(f')_j^n = (f'_0)_j^n [1 + \epsilon \sin \omega(n\Delta t)] \quad (24)$$

where  $\Delta t$  is the temporal grid size.

The initial conditions at  $t = 0$  in the  $(\zeta, \eta)$  plane correspond to the steady jet solutions of equation (19b). The finite difference equations can be obtained similar to the above derivation for the unsteady jet except terms in equation (22) at  $t = t_{n-1}$  are equal to those at  $t = t_n$  and  $\alpha_1 = 0$ .

### 3.2. Time Varying Velocity Profile at the Nozzle Exit

Because of symmetry, only half of the jet needs to be computed. The time-varying velocity profile considered at the nozzle exit is the commonly assumed "top-hat" profile which is given by

$$U(y,t) = \begin{cases} 1 + \epsilon \sin \omega t & \text{for } 0 \leq y \leq 1/2 \\ 0 & \text{for } 1/2 < y \end{cases} \quad (25)$$

In terms of the transformed coordinates, equation (25) can be rewritten using equation (17) as

$$f' = \begin{cases} \frac{(\zeta + \zeta_0)^{1/2}}{ab} (1 + \epsilon \sin \omega t) & \text{for } 0 \leq \eta \leq (\eta_\infty)_i \\ 0 & \text{for } (\eta_\infty)_i \leq \eta \end{cases}$$

$$\text{where } (\eta_\infty)_i = 0.5 a/\zeta_0 \quad (26)$$

Since a discontinuity exists in  $f'$  at  $\eta = (\eta_\infty)_i$  and will cause computational problems, the top-hat profile has to be approximated by

$$f' = \frac{(\zeta + \zeta_0)^{1/2}}{ab} \phi_1(\eta) (1 + \epsilon \sin \omega t) \quad (27)$$

where

$$\phi_1(\eta) = \begin{cases} 1 & \text{for } 0 \leq \eta \leq \eta_a \\ (1 - \eta_N^2)(1 + 2\eta_N) & \text{for } \eta_a \leq \eta \leq (\eta_\infty)_i \\ 0 & \text{for } (\eta_\infty)_i \leq \eta \end{cases} \quad (28)$$

$$\eta_N = \frac{\eta - \eta_a}{(\eta_\infty)_i - \eta_a}$$

and  $\eta_a$  is some point in the interval  $[0, (\eta_\infty)_i]$ .

The function  $(1 - \eta_N^2)(1 + 2\eta_N)$  was obtained by matching the velocity and velocity gradient profiles at  $\eta = (\eta_\infty)_i$  and  $\eta = \eta_a$  through the following boundary conditions to ensure continuity:

$$\eta_N = 0 \quad \phi_1 = 1 \quad \phi_1' = 0 \quad (29a)$$

$$\eta_N = 1 \quad \phi_1 = 0 \quad \phi_1' = 0 \quad (29b)$$

$f$  and  $f''$  can be obtained by respectively integrating and differentiating equation (27) with respect to  $\eta$  to yield

$$f = \frac{(\zeta + \zeta_0)^{1/2}}{ab} \phi_0(\eta)(1 + \epsilon \sin \omega t) \quad (30)$$

$$\text{and } f'' = \frac{(\zeta + \zeta_0)^{1/2}}{ab} \phi_2(\eta)(1 + \epsilon \sin \omega t) \quad (31)$$

$$\phi_0(\eta) = \begin{cases} 1 & \text{for } 0 \leq \eta \leq \eta_a \\ [(\eta_\infty)_i - \eta_a] \eta_N (1 - \eta_N^2 + 0.5 \eta_N^3) & \text{for } \eta_a \leq \eta \leq (\eta_\infty)_i \\ 0 & \text{for } (\eta_\infty)_i \leq \eta \end{cases} \quad (32)$$

$$\text{and } \phi_2(\eta) = \begin{cases} 1 & \text{for } 0 < \eta < \eta_a \\ -6\eta_N (1 - \eta_N) / [(\eta_\infty)_i - \eta_a] & \text{for } \eta_a \leq \eta \leq (\eta_\infty)_i \\ 0 & \text{for } (\eta_\infty)_i \leq \eta \end{cases} \quad (33)$$

The value of  $\eta_a$  can be determined to match the experimental top-hat profile as close as possible and in this study it is chosen to be the point such that the velocity profile is uniform over 97.5% of the nozzle.



Adopting similar procedure given in Lai and Simmons (1978),  
a and  $\zeta_0$  are given the values 0.3 and 3.75 respectively  
such that  $(\eta_\infty)_i = 0.04$  and  $\eta_a = 0.039$ .

### 3.3 Solution of the Finite Difference Equation

With  $(f_j^{n-1}, g_j^{n-1}, q_j^{n-1})$  known from the solution of Eq (19b) and  $(f_j^{i-1}, g_j^{i-1}, q_j^{i-1})$  specified by Eqs. (27), (30) and (31), Eq.(22) for  $1 \leq j \leq J$  and Eq. (23) yield an implicit non-linear algebraic system of  $3J + 3$  equations. This system is linearized by Newton's Method by introducing the perturbed quantities  $(\delta f, \delta g, \delta q)$  to yield after considerable algebra

$$\delta f_j - \delta f_{j-1} - \frac{h_j}{2}(\delta g_j + \delta g_{j-1}) = (r_1)_j \quad (34a)$$

$$\delta g_j - \delta g_{j-1} - \frac{h_j}{2}(\delta q_j + \delta q_{j-1}) = (r_3)_{j-1} \quad (34b)$$

$$\begin{aligned} (s_1)_j \delta q_j + (s_2)_j \delta q_{j-1} + (s_3)_j \delta f_j + (s_4)_j \delta f_{j-1} \\ + (s_5)_j \delta g_j + (s_6)_j \delta g_{j-1} = (r_2)_j \end{aligned} \quad (34c)$$

where

$$(s_1)_j = B_j + \frac{h_j}{2} (f_j + \alpha f_{j-\frac{1}{2}} + \alpha \beta_1)$$

$$(s_2)_j = B_{j-1} + \frac{h_j}{2} (f_{j-1} + \alpha f_{j-\frac{1}{2}} + \alpha \beta_1)$$

$$(s_3)_j = \frac{h_j}{2} (q_j + \alpha q_{j-\frac{1}{2}} + \alpha q_{j-\frac{1}{2}}^{234})$$

$$(s_4)_j = \frac{h_j}{2} (q_{j-1} + \alpha q_{j-\frac{1}{2}}^{234})$$

$$(s_5)_j = h_j (g_j - \alpha g_{j-\frac{1}{2}} - \frac{\alpha \beta}{2} - \frac{\alpha_1}{2})$$

$$(s_6)_j = h_j (g_{j-1} - \alpha g_{j-\frac{1}{2}} - \frac{\alpha \beta}{2} - \frac{\alpha_1}{2})$$

$$(r_1)_j = f_{j-1} - f_j + h_j g_{j-\frac{1}{2}}$$

$$(r_3)_{j-1} = g_{j-1} - g_j + h_j q_{j-\frac{1}{2}}$$

$$\begin{aligned} (r_2)_j &= T_{j-\frac{1}{2}}^{i-1,n-1} + (Bq)_{j-1} - (Bq)_j - h_j \{g_{j-\frac{1}{2}}^2 (fq)_{j-\frac{1}{2}} \\ &\quad - \alpha [\frac{1}{2}(g_{j-\frac{1}{2}}^2 + g_j g_{j-1}) + \beta g_{j-\frac{1}{2}} - f_{j-\frac{1}{2}} g_{j-\frac{1}{2}} \\ &\quad - \beta_1 q_{j-\frac{1}{2}} - q_{j-\frac{1}{2}}^{234} f_{j-\frac{1}{2}}] - \alpha_1 g_{j-\frac{1}{2}} \} \end{aligned}$$

The boundary conditions are given by

$$\begin{aligned} \delta f_0 &= 0 \\ \delta q_0 &= 0 \\ \delta g_j &= 0 \end{aligned} \tag{35}$$

The above derivation is similar to that outlined in Appendix C in Lai & Simmons (1978). The linear system Eq. (3.10) is then solved very effectively by the Block Elimination Method discussed by Cebeci and Bradshaw (1977).

The linearized form of the steady jet equation can similarly be obtained and solved with quantities at  $t = t_{n-1}$  equal to those at  $t = t_n$  and  $\alpha_1 = 0$ .

### 3.4 Convergence Criterion

As the governing equations for both the steady and unsteady jet are parabolic, they are solved by marching along the  $t$ -direction in the case of the unsteady jet and along the  $\zeta$ -direction in the case of the steady jet. At a given stream-wise ( $\zeta$ ) station, the linearized system Eq. (34) is solved by iterating at each  $t$ -station until some convergence criterion is satisfied. Iterations are terminated at each  $t$ -station if

$$|f^{(i+1)} - f^{(i)}| < \epsilon_1, \text{ at } \eta = \eta_{\text{con}} \quad (36)$$

where the value of  $\epsilon_1$  is prescribed;

$f^{(i)}$  and  $f^{(i+1)}$  are the  $i$ th and  $(i+1)$ th iterates of  $f'$  respectively; and  $\eta_{\text{con}}$  is some point where the convergence criterion is applied. In practice, it is adequate to set  $\epsilon_1$  to be  $10^{-3}$ .

### 3.5 Criterion for the Spreading of Jet

Since the mass flow varies sinusoidally with time, and because of the initially steep velocity gradient, the jet width will be changing with time at a given streamwise ( $\zeta$ ) station. A criterion must therefore be set to determine  $\eta_\infty$  at each  $t$ -station, noting that  $\eta_\infty^{(i)} \geq \eta_\infty^{(i-1)}$ . Here  $\eta_\infty^{(i)}$  and  $\eta_\infty^{(i-1)}$  are the jet width for the  $i$ th and  $(i-1)$ th iterations. The edge of the jet is defined by the following two conditions -

$$|f'_{J-1}| \leq \epsilon_2 \quad (37a)$$

$$|f''_j| \leq \epsilon_3 \quad (37b)$$

where the values of  $\epsilon_2$  and  $\epsilon_3$  are prescribed and  $J$  denotes the point at the jet boundary. Experience indicates that it is sufficient to choose

$$\epsilon_2 = 10^{-2} \quad \text{and} \quad \epsilon_3 = 10^{-1}$$

If the criteria set out in Eq. (37) are satisfied then  $\eta_\infty^{(i+1)} = \eta_\infty^{(i)}$ . Otherwise  $n_g$  points have to be added so that  $J_{\text{new}} = J_{\text{old}} + n_g$  and the values of  $(f_j^{i,n}, g_j^{i,n}, q_j^{i,n})$  for the new  $n_j$  points are obtained as follows -

$$f_j^{i,n} = (\eta_j - \eta_\infty) g_J^{i,n} + f_J^{i,n} \quad (38a)$$

$$g_j^{i,n} = g_J^{i,n} \quad (38b)$$

$$q_j^{i,n} = 0 \quad (38c)$$

$$B_j^{i,n} = B_J^{i,n} \quad (38d)$$

The same procedure is also applied to  $f_j^{i,n-1}$ ,  $g_j^{i,n-1}$ ,  
 $q_j^{i,n-1}$ ,  $B_J^{i,n-1}$ ,  $f_j^{i-1,n}$ ,  $g_j^{i-1,n}$ ,  $q_j^{i-1,n}$ ,  $B_j^{i,n-1}$ ,  $f_j^{i-1,n-1}$ ,  
 $q_j^{i-1,n-1}$ ,  $B_j^{i-1,n-1}$

### 3.6 Criterion for the Attainment of Steady State Solution

As the mass flow at the nozzle varies sinusoidally with time, the steady state solution at any streamwise ( $\zeta$ ) station downstream must vary periodically and can be expressed in the form

$$f'(\zeta, t, \eta) = f'_0(\zeta, t, \eta) + \lim_{L \rightarrow \infty} \sum_{\ell=1}^L \varepsilon_{\ell} f_{\ell}(\zeta, \eta) \sin(\ell \omega t + \phi_{\ell}) \quad (39)$$

In general, for a periodically pulsed flow, the steady state solution at a given streamwise ( $\zeta_i$ ) station, is said to be reached if

$$f'(\zeta, t + nT, \eta) = f'(\zeta, t, \eta) \quad \text{for } n = 1, 2, \dots$$

where  $T$  is the period of oscillation.

This entails velocity profiles to agree over a few cycles and thus requires unnecessary and uneconomic computations extending for a few periods in order to ascertain that steady state has been attained. However, if all the three parameters,  $f$ ,  $f'$  and  $f''$  are considered, it is adequate to regard that the steady state solution has been reached if at some point  $\eta_s$ , the following criteria are satisfied -

$$\begin{aligned} | [f(\zeta, t_n + T, \eta_s) - f(\zeta, t_n, \eta_s)] / f(\zeta, t_n, \eta_s) | &\leq \varepsilon_4 \\ | [f'(\zeta, t_n + T, \eta_s) - f'(\zeta, t_n, \eta_s)] / f'(\zeta, t_n, \eta_s) | &\leq \varepsilon \quad n = 1, 2 \quad (40) \\ | [f''(\zeta, t_n + T, \eta_s) - f''(\zeta, t_n, \eta_s)] / f''(\zeta, t_n, \eta_s) | &\leq \varepsilon_6 \end{aligned}$$

where the values of  $\epsilon_4$ ,  $\epsilon_5$  and  $\epsilon_6$  are prescribed and  $t_2 - t_1 = \Delta t$ .

The sensitivity of the steady-state test varies with the point  $\eta_s$  to which it is applied. In practice, the point  $\eta_s$  should be so chosen such that reasonable sensitivity is achieved without excessive computations.

Since  $f'$  and  $f''$  are the first and second order derivatives of  $f$ , discrepancies between results separated by one period  $T$  are more pronounced in  $f''$ . Hence, in general  $\epsilon_4$ ,  $\epsilon_5$  and  $\epsilon_6$  must be so chosen that  $\epsilon_4 \leq \epsilon_5 \leq \epsilon_6$ . Otherwise, if  $\epsilon_6 > \epsilon_5 > \epsilon_4$  and if  $\epsilon_6$  is very small, the criteria in Eq. (40) might never be satisfied although the steady state solution has long been attained within practical limits.

As a further check of the attainment of the steady-state condition, the following condition is imposed on  $f'$  at the centre-line -

$$|[f'(\zeta, t_n + T, 0) - f'(\zeta, t_n, 0)]/f'(\zeta, t_n, 0)| \leq \epsilon_7 \quad (41)$$

for  $n = 1, 2$

where the value of  $\epsilon_7$  is prescribed.

It has been chosen that  $\epsilon_4 = \epsilon_5 = \epsilon_6 = \epsilon_7 = 10^{-2}$



### 3.7 Mean Momentum Flux, Phase Angle and Peak-to-Peak Oscillation

#### 3.7.1 Mean Momentum Flux

The instantaneous momentum at a specified streamwise ( $\zeta_i$ ) station is given by

$$M_i = 2hU_{ci}^2 \int_0^{\eta_\infty} [f'(\zeta, t_i, \eta)]^2 d\eta \quad (42)$$

$M_i$  is evaluated by Simpson's rule for unequally spaced points derived in Appendix D in Lai & Simmons (1978).

The mean momentum flux in the streamwise direction is defined by

$$M = \frac{1}{T} \int_{t_0}^{t_0 + T} M_i dt \quad (43)$$

and the integral is approximated by

$$M = \frac{1}{N} \sum_{i=1}^N M_i \quad (44)$$

The quantity  $M$  can be served as an additional check on the overall results by testing for its constancy with  $\zeta$ .

#### 3.7.2. Phase Angle

The phase angle between the fundamental component of the centre-line velocity at any downstream station and that at the nozzle can readily be obtained by cross-correlating the steady-state instantaneous centre-line velocity at that station with a reference sine and cosine signal respectively.

Consider

$$S_1 = \sin \omega t \quad (45)$$

$$S_2 = \cos \omega t \quad (46)$$

From Eq. (39),

$$f'_C \equiv f'(\zeta, t, 0) = f'_0(\zeta, t, 0) + \lim_{L \rightarrow \infty} \sum_{\ell=1}^L \epsilon^\ell f_\ell(\zeta, 0) \sin(\ell\omega + \phi_\ell) \quad (47)$$

Multiplying Eq. (45) with Eq. (47) and taking time average yields

$$\overline{S_1 f'_C} = A \cos \phi_1 \quad (48)$$

where A is a constant.

Multiplying Eq. (46) with Eq. (47) and taking time average gives

$$\overline{S_2 f'_C} = A \sin \phi_1 \quad (49)$$

From Eqs. (48) and (49),

$$\phi_1 = \tan^{-1} \frac{\overline{S_2 f'_C}}{\overline{S_1 f'_C}} \quad (50)$$

### 3.7.3. Peak-to-Peak Oscillation

The percentage peak to peak variation of the centre-line velocity at any downstream station is defined by

$$F = \frac{(f'_C)_{\max} - (f'_C)_{\min}}{\overline{f'_C}} \times 100\% \quad (51)$$

The quantities  $(f'_c)_{\max}$  and  $(f'_c)_{\min}$  are obtained by quadratic interpolation of the form

$$f'_c = a_0 t^2 + a_1 t + a_2 \quad (52)$$

through three points  $(f'_c(t_1), t_1)$ ,  $(f'_c(t_2), t_2)$  and  $(f'_c(t_3), t_3)$

where for  $(f'_c)_{\max}$ ,  $f'_c(t_1) \leq f'_c(t_2)$

$$f'_c(t_3) \leq f'_c(t_2)$$

and for  $(f'_c)_{\min}$   $f'_c(t_1) \geq f'_c(t_2)$

$$f'_c(t_3) \geq f'_c(t_2)$$

Eq. (52) can be solved for  $a_0$ ,  $a_1$  and  $a_2$  by substituting  $f'_c(t_1)$ ,  $f'_c(t_2)$  and  $f'_c(t_3)$ . With  $a_0$ ,  $a_1$  and  $a_2$  known,  $(f'_c)_{\max}$  or  $(f'_c)_{\min}$  can be obtained from Eq. (52) with  $t$  given by  $-a_1/2a_0$ .

#### 4.0 Results and Discussions

The structure and listing of the computer programs for both the steady and unsteady jet are described in Appendix A. Calculations were performed on the University of Queensland PDP1055 and the U.S. Naval Postgraduate School IBM 360/67 computers. The computer program for the steady jet occupies a core memory of 16K words and that of the unsteady jet occupies a core memory of 67K words. It must be pointed out here that the unsteady jet program can actually be reduced to about 25K words of core memory since at any one time instant, only calculations involving two time levels are required in core whereas all the quantities at other time levels can be stored on disk and retrieved when required. However, in this case, the computer core storage is not a problem with the computing facility available whereas the computing time is important and as such a trade-off is made such that quantities at all time levels are retained in core in order to save computing time of writing to and reading from disk. Moreover, although a constant eddy viscosity model was used, the programs were written to accept variable eddy viscosity. A very straightforward modification of the program by incorporating a routine to read from and write to a disk can reduce its size to enable it to be run on any mini-computer with available core memory of about 25K words.

#### 4.1 Steady Jet

Owing to the nature of the initially top-hat velocity profile, the initial velocity gradient is very steep and the velocity profile changes vary appreciably over a very short streamwise distance. Since the solution of the finite difference equations is obtained through linearization by Newton's method as described in section 3.3, an initial guess at any streamwise station must be close to the solution. Consequently, a fine grid has also to be used initially but as the computation proceeds and as the velocity profiles start to appear in similar form, a coarser grid can be used by dropping every other point. The initial grid used in the transverse ( $\eta$ ) direction is specified as follows:

$$\begin{array}{rcl}
 & 0.005 & 0 \leq \eta \leq 0.01 \\
 & 0.002 & 0.01 \leq \eta \leq 0.036 \\
 & 0.0002 & 0.036 \leq \eta \leq 0.039 \\
 \Delta\eta = & 0.0001 & 0.039 \leq \eta \leq 0.04 \\
 & 0.00025 & 0.04 \leq \eta \leq 0.045 \\
 & 0.001 & 0.045 \leq \eta \leq 0.06 \\
 & 0.002 & 0.06 \leq \eta \leq 0.02 \\
 & 0.01 & \eta \leq 0.12 \\
 (\eta_{\infty})_i = & 0.04 & 
 \end{array} \tag{53}$$

The grid-sizes in the streamwise ( $\zeta$ ) direction are specified as follows:

$\Delta \zeta =$	0.0005	$0 \leq \zeta \leq 0.007$	
	0.005	$0.007 \leq \zeta \leq 0.032$	
	0.025	$0.032 \leq \zeta \leq 0.132$	
	0.1	$0.132 \leq \zeta \leq 1.032$	
	1	$1.032 \leq \zeta \leq 20.032$	(54)
	2	$20.032 \leq \zeta \leq 40.032$	
	5	$40.032 \leq \zeta$	

The constants  $c_1$  and  $c_2$  in equation (12) in the constant eddy viscosity model are varied to match the experimental data. The sensitivity of the solutions to various values of  $c_1$  and  $c_2$  was tested. No significant difference was found when  $c_1$  was varied from 0.009 to 0.012 and  $c_2$  from 0.032 to 0.037. The final values of  $c_1 = 0.009$  and  $c_2 = 0.034$  were chosen.

As shown in Fig. 3, the non-dimensional self-preserved velocity profiles of various workers agree very well with each other and with the Goertler solution except near the jet edge where conventional hot-wire measurements are dubious. However, the results of Heskestad (1965) follow very closely the Goertler solution and those of Robins (1971) which have been recommended by Rodi (1975) as reliable agree very well with the results of Heskestad (1965). The computed development of the non-dimensional velocity profiles of the steady jet with  $y$  normalized with respect to the jet half-width  $y_{1/2}$  are depicted in Fig. 4 and at streamwise station  $\zeta = 22.032$ , the mean velocity profile differs insignificantly from

the Goertler solution, indicating that self-preservation in mean velocity profile is attained.

The variation of the non-dimensional centre-line velocity with streamwise distance is plotted in Fig. 5. The results agree well with the experimental data of Lai and Simmons (1979) and Zijnen (1958). The variation of the jet half-width with streamwise distance is compared with the result of Kotsovinos (1976) and Lai and Simmons (1979) in Fig. 6 and is found to give reasonably good agreement for streamwise distance less than about 40 nozzle widths. The discrepancy which exists at larger streamwise distance is not as significant as it appears because the results of Kotsovinos (1976) were obtained by fitting a third-order polynomial through the scattered data in the literature and most of the experimental data were not available for streamwise distance larger than 50 nozzle widths. Furthermore, uncertainty in the hot-wire data increases as the streamwise distance increases because of the decay of the velocity profile and possible three-dimensional and reversed flow effects. The rate of decay of the centre-line velocity  $d \bar{U}_C^2 / d(x/h)$  of 0.165 and the spreading rate  $d(y_{1/2}/h) / d(x/h)$  of 0.106 obtained from Figs. 5 and 6 respectively fall within the range of values reported in the literature. As pointed out by Goldschmidt and Bradshaw (1980), exact self-preservation in mean quantities requires the kinematic virtual origin, obtained from the centre-line velocity decay curve, be equal to the geometric virtual origin obtained from the jet spreading curve. However, most

experimental data do not confirm this. In this study, the computed kinematic virtual origin agrees with the geometric virtual origin and is found to be  $0.8h$ .

The development of the normalized shear stress profiles is shown in Fig. 7. The agreement between the computed shear stress profile at  $\zeta = 95.032$  and the experimental results of Gutmark and Wagnanski (1976) is good considering that the shear stress term is the most difficult to be measured with sufficient accuracy and a scatter of at least 20% exists in the available experimental data in the literature. The maximum value of the computed non-dimensional shear stress term  $\overline{u'v'}/U_c^2$  is 0.023 which agrees well with most measured values reported in Rodi (1975).

In jet computations, numerical errors introduced at the jet edge normally have little overall influence on the calculations as noted by McGuirk and Rodi (1979). The momentum integral in this study varies by less than 1% over a streamwise distance of 100 nozzle widths.



## 4.2 Unsteady Jet

The constant eddy-viscosity model which was found to give good agreement with experimental data was used in the computation of the preiodically pulsed jet. Results were obtained for three frequencies of pulsation,  $\omega = 0.000871$ ,  $0.00871$  and  $0.0871$  which for a jet exit Reynolds number of  $10^4$  and a jet width  $h$  of  $5\text{mm}$  correspond to  $1$ ,  $10$  and  $100$  Hz respectively. Two values of amplitude of pulsation were studied, namely  $\epsilon = 0.1$  and  $0.15$ . The results were compared with the experimental data of Lai and Simmons (1979) and solutions for steady jets. The grid-sizes used in the streamwise ( $\zeta$ ) and transverse ( $\eta$ ) directions are the same as those of the steady jet given in section 4.1.

### 4.2.1 Sensitivity of the Solution to the Convergence Criterion

Results show that solutions are very sensitive to the convergence criterion applied to points very near to the edge of the jet. Normally, the closer the point  $\eta_{\text{con}}$  is to the edge of the jet, the more difficult it will be for the solution to converge. It was found by Lai and Simmons (1979) that the convergence criterion can be applied to a point in the jet which varies with streamwise distance and is defined by

$$\eta_{\text{con}} = \begin{cases} (\eta_{\infty})_i - 3 & \text{for } \zeta \leq 0.1 \\ 5(\eta_{\infty})_{\text{min}}/10-1 & \text{for } \zeta \geq 0.1 \end{cases} \quad (55)$$

This allows a comparatively sensitive measure of the convergence of the solution and yet maintains a reasonably

fast convergence without affecting the overall accuracy of the solution.

A fixed point arbitrarily defined by  $\eta_{\text{con}} = \eta_{\infty} - 6$  may also be sufficient.

#### 4.2.2 Validity of the Criterion for the Attainment of Steady State Solution

The criterion for the attainment of steady state solution described in section 3.6 is found to be adequate. The point  $\eta_s$  to which the steady state tests are applied has been chosen to coincide with  $\eta_{\text{con}}$  specified in equation (53).

#### 4.2.3 Sensitivity of the Solution to Time Step

The sensitivity of the solution to time step has been tested for various frequencies. Calculations have been carried out with the period of pulsation divided into 12, and 49 intervals respectively. Results indicate that although division of a period into 12 time intervals seems to be too coarse, they differ insignificantly from each other. It is therefore sufficient to use 12 time intervals in the present study.

#### 4.2.4 Relaxation of the Criterion for Jet Spreading

As pointed out in section 3.5, the jet spreads rapidly initially due to a steep velocity gradient. As the computations proceed downstream, the velocity profile becomes wider with a long tail at the jet edge. Because of the very low velocities at the jet edge, small numerical errors introduced there might cause instabilities and the criteria set out in equation (37) for the definition of the jet edge will not be satisfied resulting in continuous addition of unnecessary grid points. Furthermore, the number  $n_g$  of grid points which can

be added each time imposes a trade-off between the accuracy of the solution and the computing time required. This is because less computing time will be required if more points are added but since the quantities at the new points are obtained by extrapolation and the jet edge is particularly sensitive to small numerical errors, instability or inaccurate solution may result. The program provides choices of two different number of added grid points as the calculations are marched downstream and if the jet spreads beyond a certain  $n$  value which can be obtained from the Goertler solution, a new definition for the jet edge is applied to terminate the jet at the point where the velocity starts increasing or changes sign.

#### 4.2.5 Results

Non-dimensional mean and instantaneous velocity profiles at various time delay intervals are plotted in Fig. 8 for the various frequencies and amplitudes of pulsation and  $\zeta = 40.032$ . The mean velocity profiles follow closely the steady jet curve. The instantaneous profiles also collapse into the steady jet curve except in Figs. 8(e) and (f) where a slight discrepancy occurs for  $\omega = 0.00871$  and  $0.0871$  and  $\epsilon = 0.15$ . This agrees with the trend observed in the experimental data of Lai and Simmons (1979), in which a slight departure of the non-dimensional instantaneous velocity profiles from the steady jet curve exists.

The mean centre-line velocity  $U_c$  obtained by time-averaging the steady state instantaneous centre-line velocity  $U_c$  over a period is shown in Fig. 9 to agree well with the centre-line velocity

decay curve for the steady jets for all the computed cases. Fig. 10 shows the variation of the jet half-width of the mean velocity profile with streamwise distance. For all cases, the mean jet half-width of the unsteady jet collapses on the steady jet spreading curve. A plot of  $Q/Q_E$ , a measure of mean entrainment, versus  $\zeta$  for various frequencies and amplitudes of pulsation indicates that the mean entrainment rate does not differ from that of the steady jet, which is consistent with the trend associated with the mean centre-line velocity decay and jet spreading. In all the computed cases, the mean momentum flux  $M$  is conserved to within 1% over a streamwise distance of 100 nozzle widths, thus confirming the accuracy of the solutions.

With reference to Fig. 12, the non-dimensional mean shear stress profiles of the unsteady jet at  $\zeta = 40.032$  agrees very well with that of the steady jet. The non-dimensional instantaneous shear stress profiles can also be collapsed into the steady jet profile except for  $\omega = 0.0871$  in Figs. 12(c) and (f) where significant discrepancies are noted. This is consistent with the behavior of the instantaneous velocity profiles where a slight disagreement will be amplified in the velocity gradient term which is shown up in the shear stress profile.

Fig. 13 shows the variation of the steady-state instantaneous centre-line velocity with time for various frequencies and amplitudes of pulsation at three different streamwise distances. The reference signal is given by

$\bar{U}_c (1 + \epsilon \sin \omega t)$ . It can be noted that as the frequency and amplitude increases and for large streamwise distance, distortions in the waveform of the centre-line velocity exist, an indication of the importance of higher harmonics. Such a trend was also observed by Lai and Simmons (1979) in their experimentally pulsed jet. The variation of the phase angle  $\phi$  between the steady-state fundamental component of the centre-line velocity at any streamwise station and that at the nozzle exit with  $\zeta$  is depicted in Fig. 14. The phase angle is a lag which increases with both frequency and streamwise distance. However, the amplitude of pulsation does not have any significant effect on the phase lag variation. For a region sufficiently close to the nozzle, the flow varies with time in a quasi-steady manner. That is, the solution over the region of interest can be approximated by a sequence of steady jet solutions, each of which corresponds to the instantaneous conditions at the nozzle. The region over which quasi-steady approximations can be applied to an unsteady jet can readily be determined by using the phase plot in Fig. 14. It is taken arbitrarily here that a phase lag of 5 degrees defines the downstream limit to quasi-steady solutions. This definition enables the quasi-steady approximations to  $\bar{U}_c$  to be accurate to within 1%. From Fig. 14 it is apparent that the region over which quasi-steady approximations can be used decreases with increasing frequency. The quasi-steady region for the computed frequencies and for  $\epsilon = 0.1$  or  $0.15$  is as follows -

$$\omega = 0.000871 \quad 0 \leq \zeta \leq 60$$

$$\omega = 0.00871 \quad 0 \leq \zeta \leq 10$$

$$\omega = 0.0871 \quad 0 \leq \zeta \leq 1$$

The variation of the percentage peak-to-peak oscillation,  $F$ , of the steady-state instantaneous centre-line velocity expressed as a percentage of the mean value with streamwise distance is plotted in Fig. 15. Although for  $\omega = 0.0871$ ,  $F$  differs quite significantly from its initial value of 20% or 30%, it varies very little for other tested frequencies and amplitudes of pulsation. In the experimental data of Lai and Simmons (1979), it was shown that for frequencies between 1 and 10 Hz, which correspond to  $\omega = 0.000871$  and 0.00871 here, the general trend indicates that  $F$  increases to a maximum at 10 nozzle widths and drops off beyond that point and  $F$  increases by almost 40% over the initial value even for 1Hz case. The present computations using the constant eddy viscosity model fail to predict this trend.

### 5.0 Concluding Remarks

A method which employs a transformation to solve the thin shear layer equations for the steady and unsteady, two-dimensional turbulent free jet issuing into stationary air has been presented. A Prandtl type constant eddy viscosity formulation was used to model the Reynolds shear stress term. The transformation reduces the rate of spread of the jet and enables the use of variable grid sizes over predetermined regions leading to accurate predictions.

In the steady jet, the mean velocity profiles, the mean centre-line velocity decay rate, the spreading rate of the jet and the normalized shear stress profiles all show good agreement with experimental data.

In the unsteady jet, the mean flow characteristics, such as the mean velocity and shear stress profiles, the mean centre-line velocity decay, the mean jet spreading and entrainment all follow closely those of the steady jet for the range of tested frequencies and amplitudes of pulsation. This is in agreement with the only available experimental data of this type which are available in Lai & Simmons (1979). However, unsteady effects are apparent in the distortion of the waveform for the variation of the instantaneous centre-line velocity with time and in the increase in the phase lag with streamwise distance. For high frequencies and amplitude of pulsation or at large streamwise distance from the nozzle, instantaneous quantities depart from quasi-steady values. The flow region over which quasi-steady approximations are applicable has been established for various frequencies.

Although the constant-eddy viscosity model used gives good predictions for the steady jet and the mean quantities for the unsteady jet, it fails to predict accurately the instantaneous quantities especially the percentage peak to peak oscillation of the steady-state instantaneous centre-line velocity. This suggests that if only mean flow quantities are required and if the frequencies and amplitudes of pulsation are of the order of those in this study, the constant eddy-viscosity model is adequate. However, if instantaneous quantities are critical and if frequencies and amplitudes of pulsation are an order of magnitude higher than those in this study, a more refined turbulence model has to be sought and tested.



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## Appendix A Structure and Listings of Computer Program

### A.1 Sturcture of the Steady Jet Program

The structure of the input data is as follows:

CARD 1	NRG, (RG(I), I = 1, NRG), DEGR
FORMAT	I5, 6F10.6
CARD 2	PROD , CONST 1, CONST 2
FORMAT	3F10.6
CARD 3	CO, XO, AA, BB, NPG, INC, IFREQ, NXI
FORMAT	4F10.6, 4I4
CARD 4	(NXTT(I), I = 2, NXII)
FORMAT	10I4
CARD 5	(DELX(I), I=1,NXI), X(1)
FORMAT	8F10.6
CARD 6	(DETAC(I), I = 1,8)
FORMAT	8F10.6
CARD 7	(VC(I), I = 1,7), ETAE
FORMAT	8F10.6
CARD 8	E1, E2, E3
FORMAT	3F10.6
CARD 9	OUTDSK, LN
FORMAT	L1, I3
CARD 10	ETAG
FORMAT	F10.6

The symbols used have the following meaning:

NRG	No. of times grid points have to be rearranged
RG(I)	Upper $\eta$ value above which grid points will not be dropped
DEGR	Lower $\eta$ value below which grid points will not be dropped.
PROD	$V$ defined in section 2.1 (Jet Exit Reynolds Number)
CONST 1, CONST 2	$c_1$ and $c_2$ defined in Eq. (12)
CO	$\zeta_0^{1/2}/(ab)$
XO	$\zeta_0$
AA	$a$ defined in Eq. (15a)
BB	$b$ defined in Eq. (15b)
NPG	$n_g$ , No. of grid points to be added if the jet spreads
INC	interval, in terms of the number of transverse grid points, at which a value of the velocity profile is required
IFREQ	interval, in terms of the number of streamwise stations, at which velocity profile is required
NXI	No. of different grid sizes in streamwise direction
NXTT(I)	Streamwise station number at which a different grid size is used.
DELX (I)	Streamwise grid size $\Delta\zeta_i$
X(1)	Value of $\zeta$ at initial streamwise station (zero at nozzle exit)
DETAC(I)	Transverse grid size $\Delta\eta$
VC(I)	Values of $\eta$ for each sub-region
ETAE	$(\eta_\infty)_i$
E1	Convergence limit defined in Eq. (36)
E2, E3	Jet edge definition defined in Eq. (37)

OUTDSK      Assumes logical value TRUE if solutions are  
             written to disk

LN            Device number of writing to disk

ETAG         $\eta_a$  defined in Eq. (28)

## ~~A.2. Listing of Steady Jet Programs~~

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### A.3 Structure of the Unsteady Jet Program

The structure of the input data is as follows:

CARD 1	NRG, (RG(I), I = 1, NRG), DEGR
FORMAT	I5, 6F10.6
CARD 2	(NXG(I), I = 1, NRG)
FORMAT	5I5
CARD 3	NPG, NPG2, START, LN, NEW, NTRANS, NPRINT
FORMAT	7I5
CARD 4	CONST 1, CONST 2
FORMAT	2F10.4
CARD 5	CO, XO, EPS, OMG, NT, INC
FORMAT	4F10.4, 2I5
CARD 6	IFREQ, IFR, IFA, NXI
FORMAT	4I5
CARD 7	(NXTT(I), I=2, NXII)
FORMAT	10I5
CARD 8	(DELX(I), I = 1, NXI), X(1)
FORMAT	8F10.4
CARD 9	(DETAC(I), I = 1,8)
FORMAT	8F10.4
CARD 10	(VC(I), I = 1,7), GTAG
FORMAT	8F10.4
CARD 11	E1, E2, E3, E4, E5, AA, BB, PROD
FORMAT	8F10.4
CARD 12	ETAG
FORMAT	F10.4

Symbols which appear also in the steady jet program have the same meanings here. All other symbols are defined as follows: -

NXG(I)	Streamwise station at which grid has to be rearranged.
NPG 2	Second choice of number of transverse grid points to be added if jet spreads as discussed in section 4.2.4
START	Streamwise station number at which computations start
NEW	See below
NTRANS	Streamwise station number at and beyond which constant $c_2$ is used.
NPRINT	Streamwise station number at and beyond which velocity profiles are required
EPS	$\epsilon$ , amplitude of pulsation
OMG	$\omega$ , angular frequency of pulsation
NT	Number of time intervals in a period + 1
IFR	interval, in terms of the number of streamwise stations, at which instantaneous velocity profiles are required.
IFA	interval, in terms of the number of streamwise stations, at which mean quantities are required
E4	$\epsilon_4$ , $\epsilon_5$ and $\epsilon_7$ defined in Eq. (40) and (41)
E5	$\epsilon_6$ defined in Eq. (40)

Because of the initially steep velocity gradient, the velocity gradient curve behaves erratically at the region around the initial jet edge which constitutes about 3% of the total jet-width. To eliminate such numerical erratic behavior, a first-order smoothing function can be applied and is supplied through the Subroutine SMOOTH. The use of the



smoothing function does not affect the overall results and is optional. The parameter NEW specifies the streamwise station number where smoothing function starts to be used. If smoothing function is not required, NEW can assume the value of the final streamwise station number.

#### A.4 Listing of Unsteady Jet Program

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# Appendix B. Figures

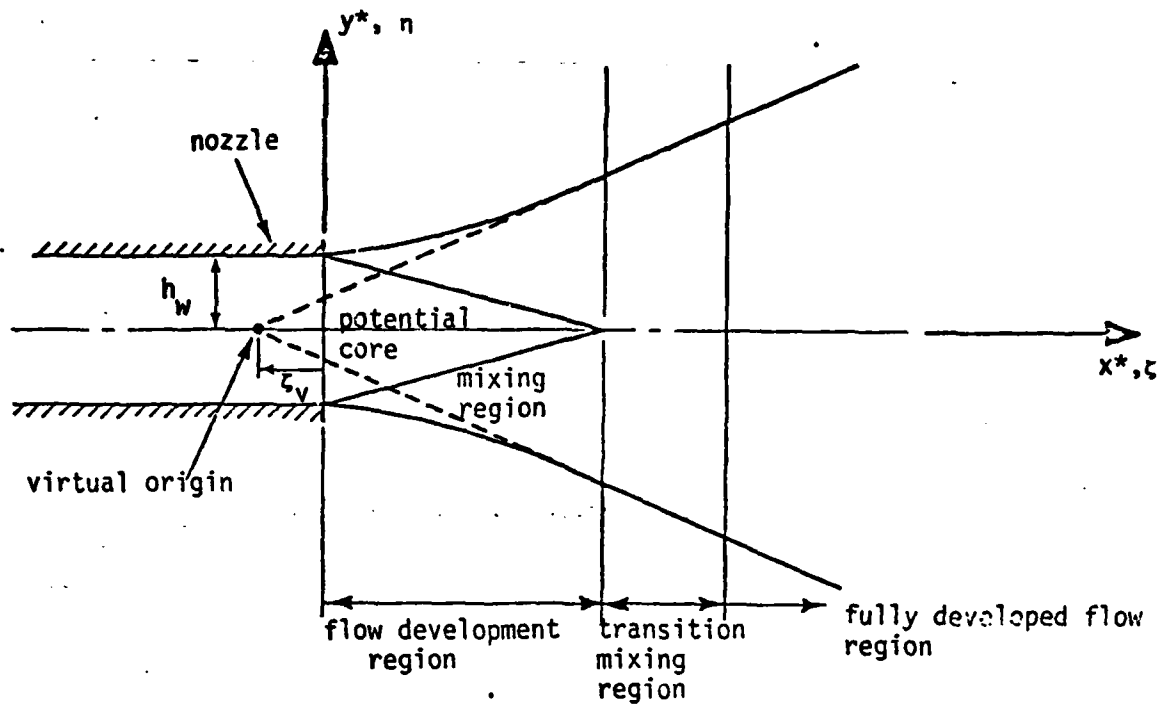


Figure 1. Configuration of the Plane Jet

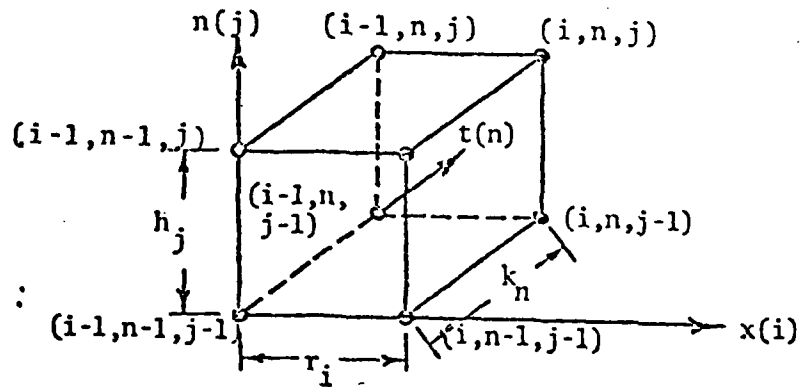


FIGURE 2. Net cube for the difference equations for Eq (21).

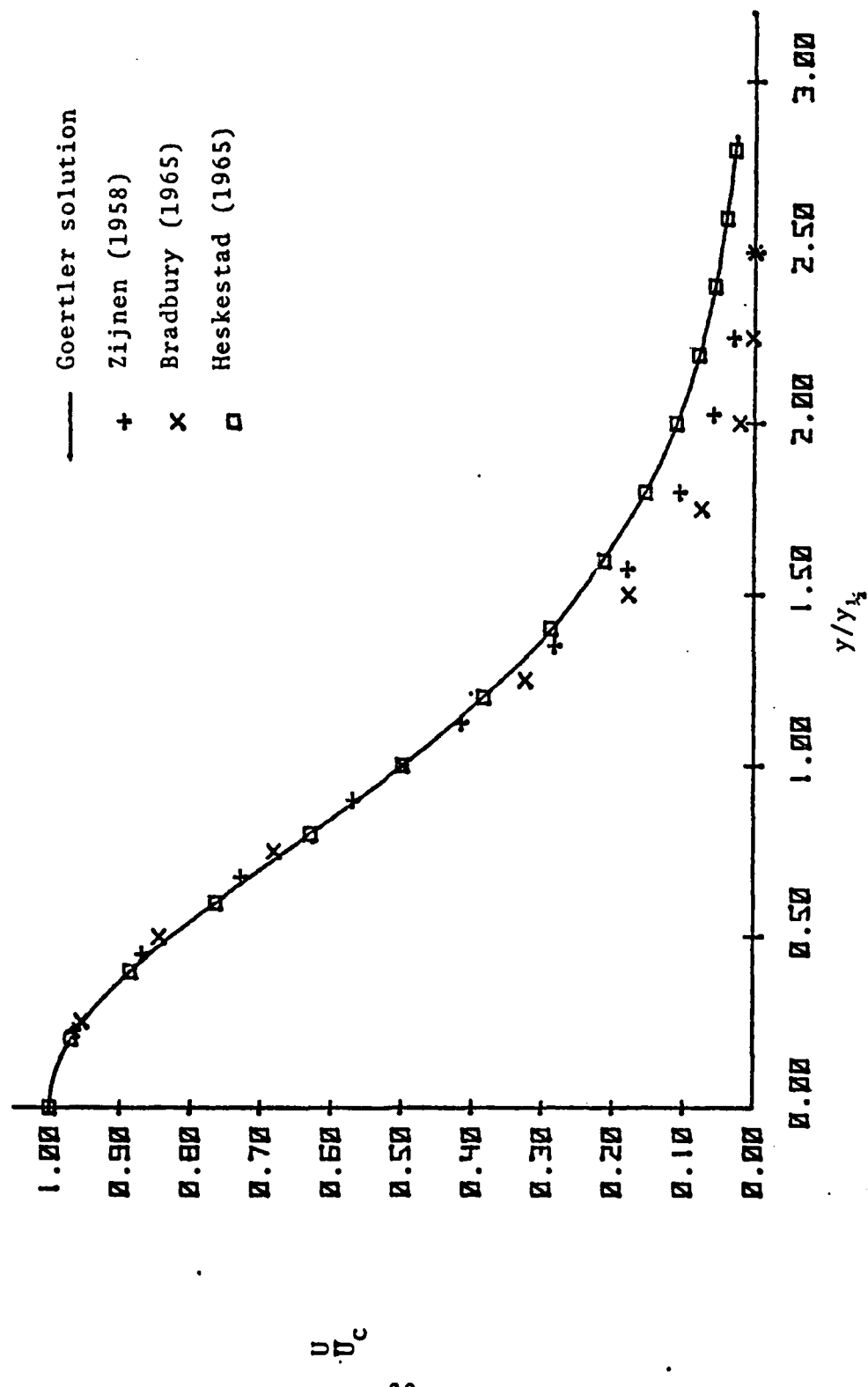


Figure 3. Non-Dimensional Self-Preserved Velocity Profile of the Steady Jet

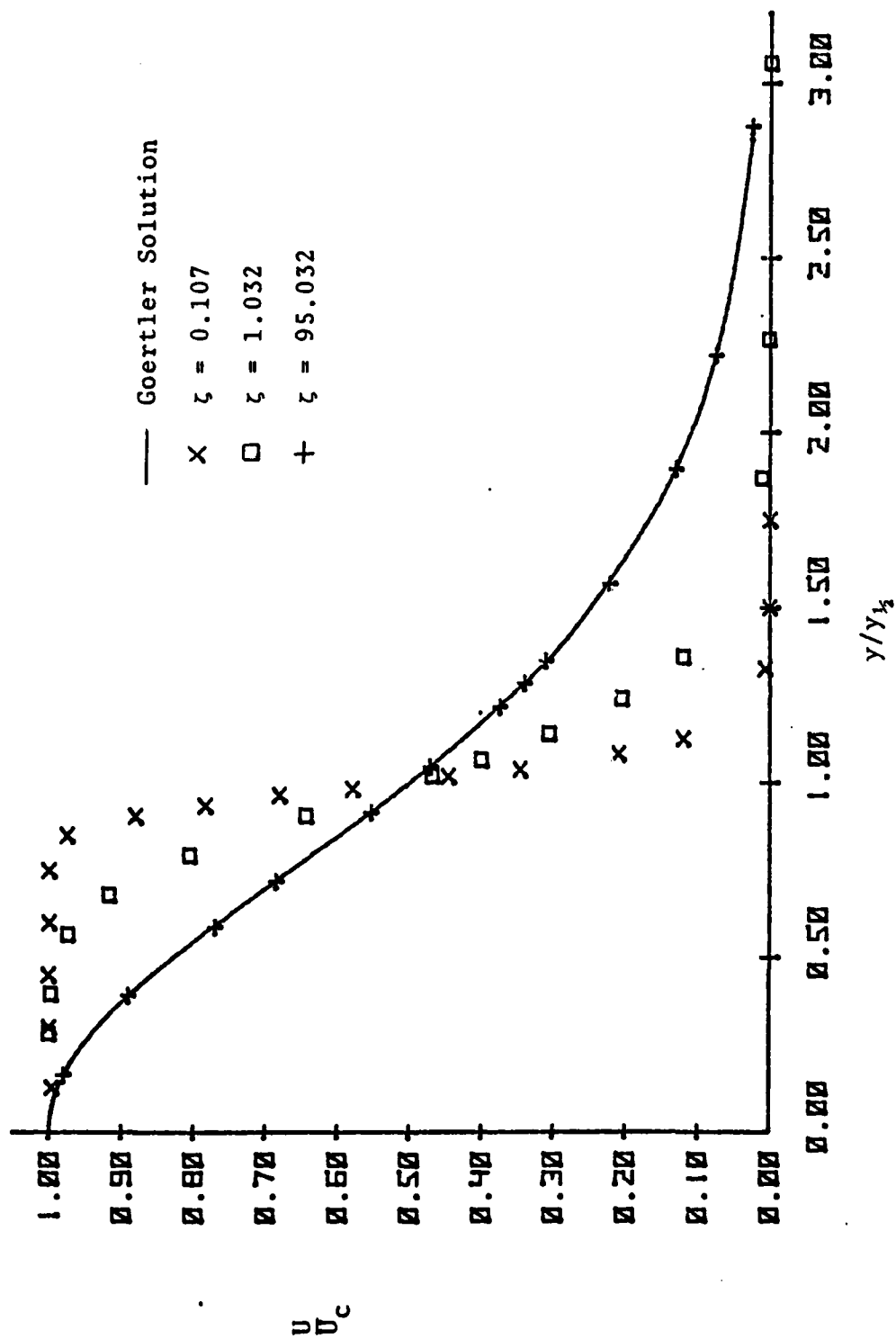


Figure 4(a) Non-Dimensional Velocity Distribution of the Steady Jet

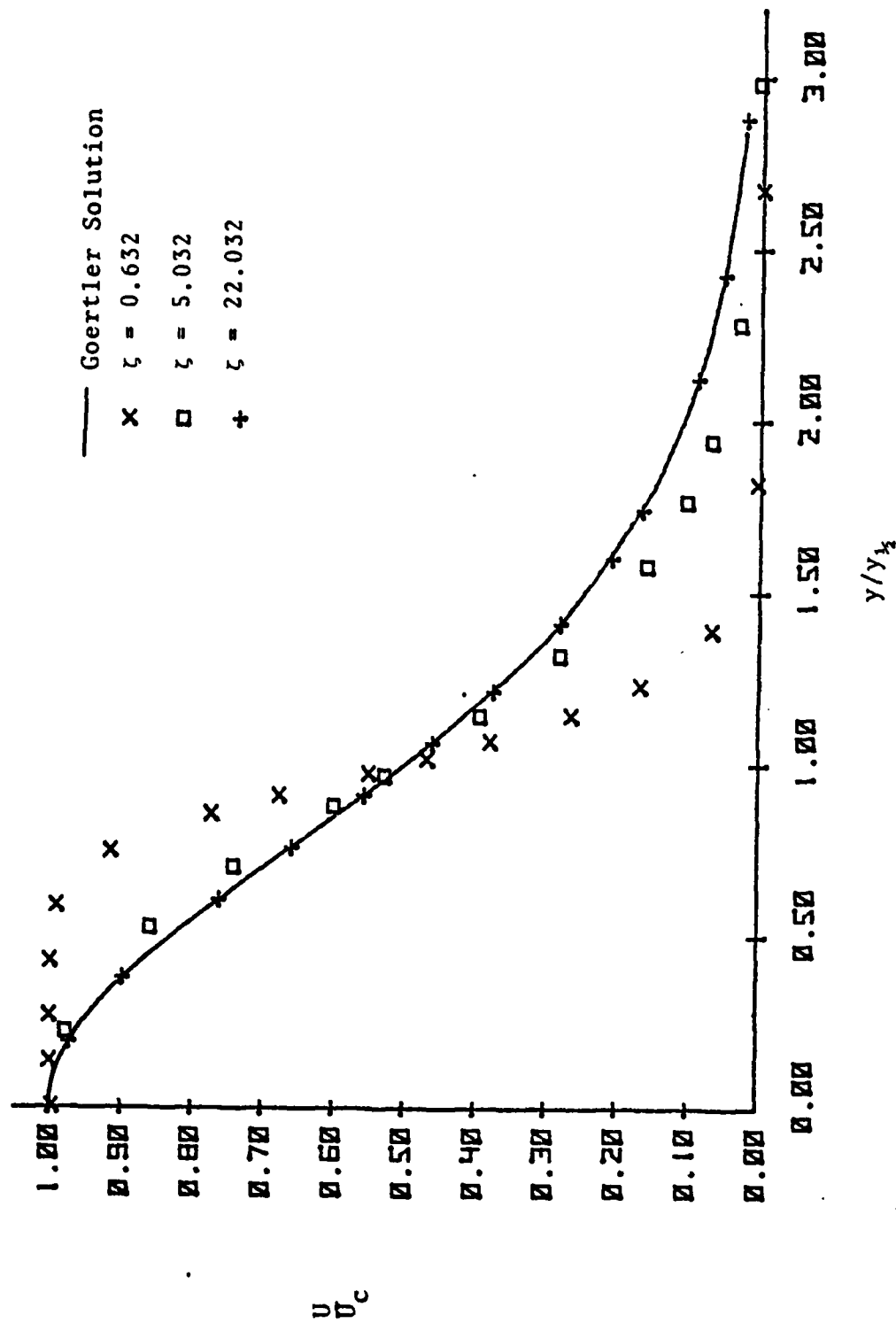


Figure 4(b) Non-Dimensional Velocity Distribution of the Steady Jet

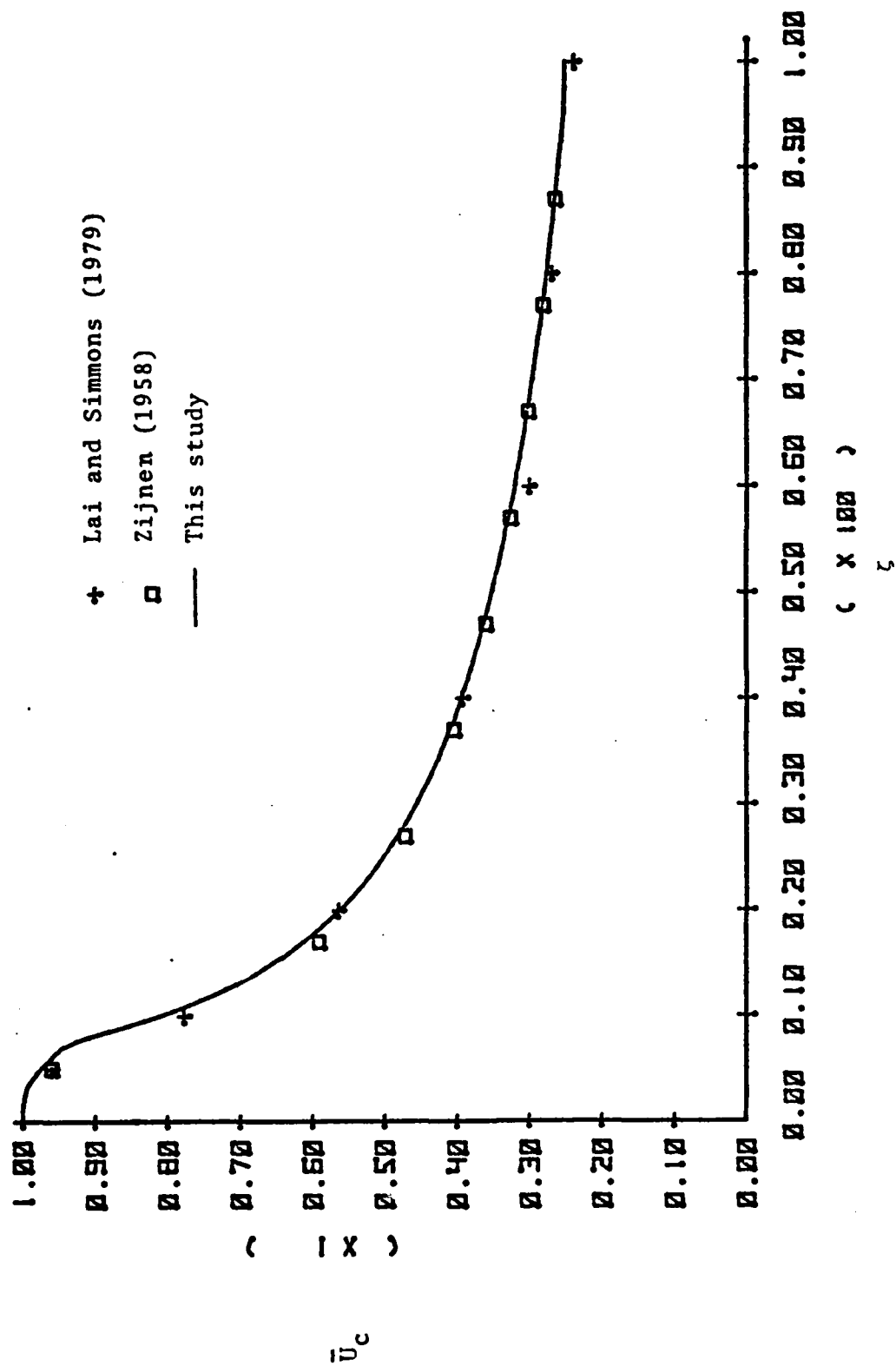
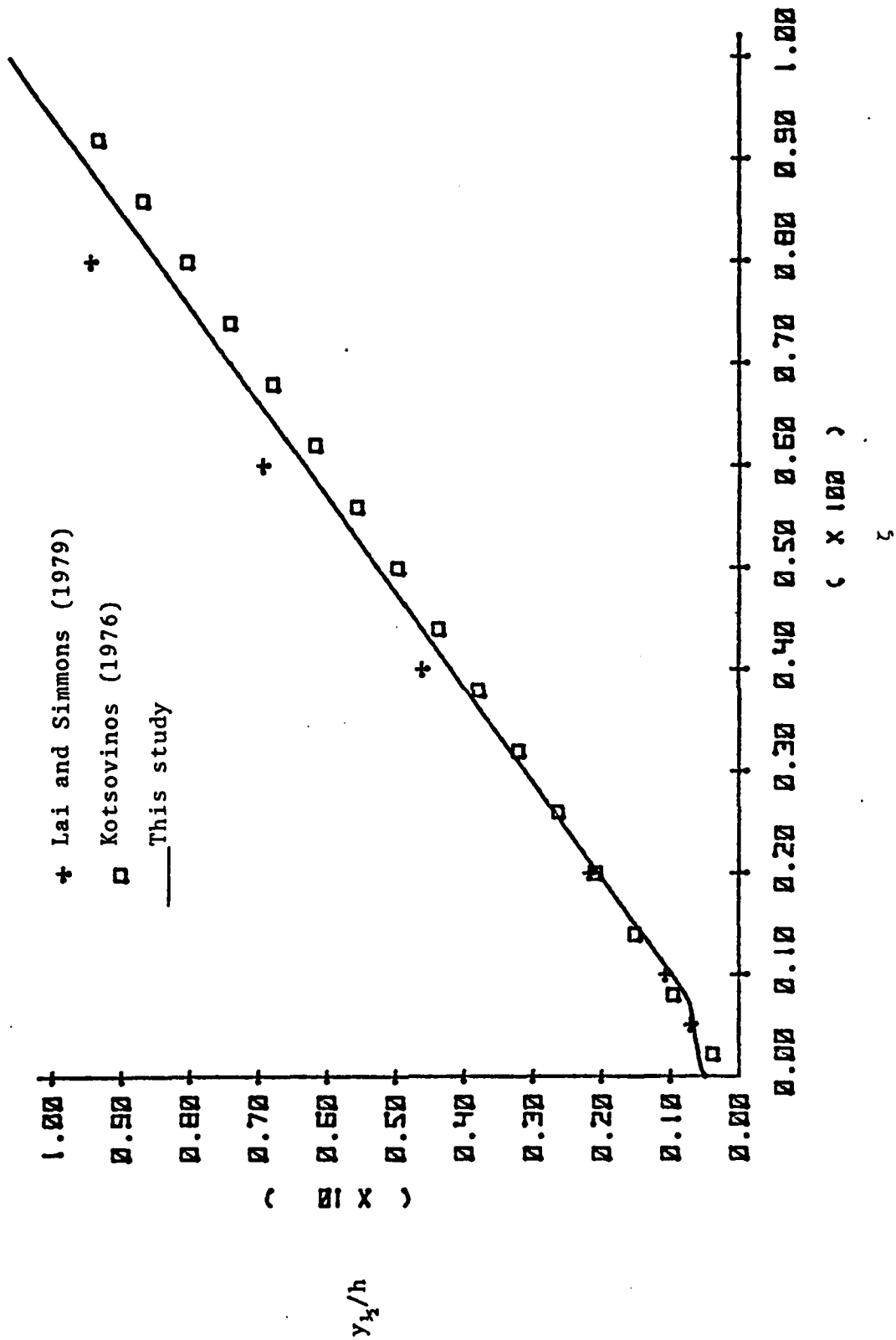


Figure 5 Variation of Centre-Line Velocity of the Steady Jet with Streamwise Distance



• Figure 6 Variation of the Half-Width of the Steady Jet with Streamwise Distance

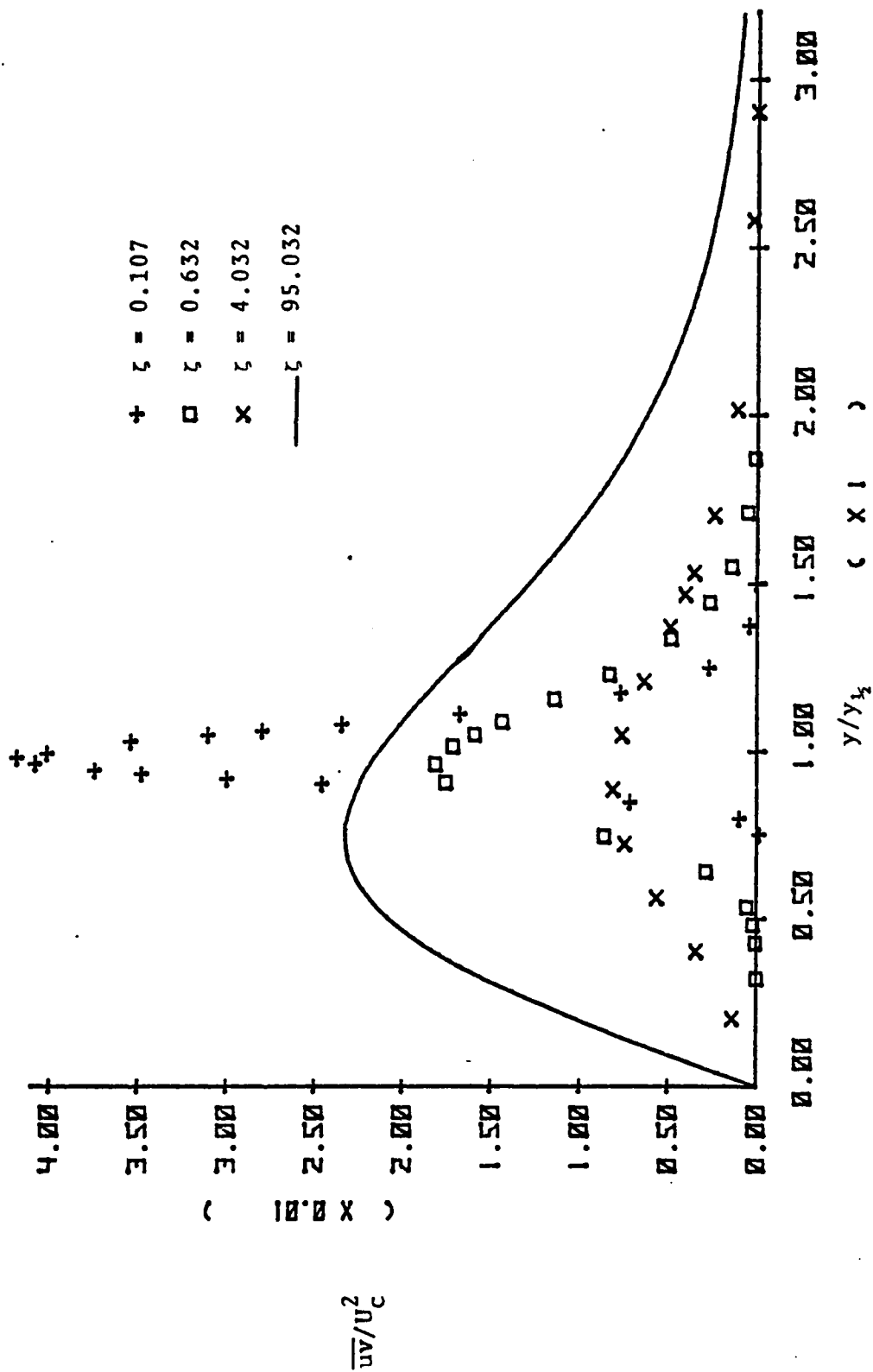


Figure 7(a) Nondimensional Shear Stress Profile for the Steady Jet



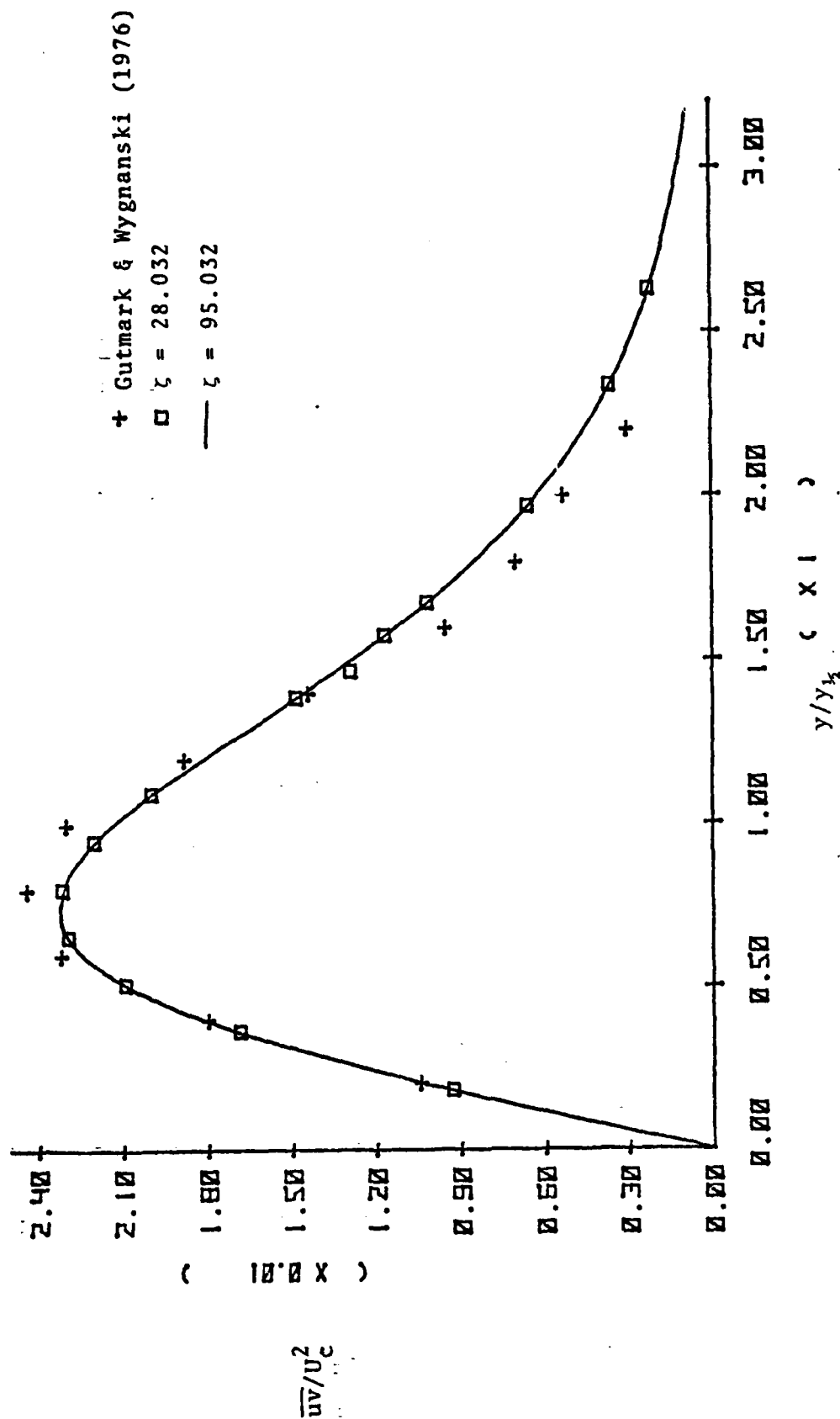


Figure 7(b) Nondimensional Shear Stress Profile for the Steady Jet

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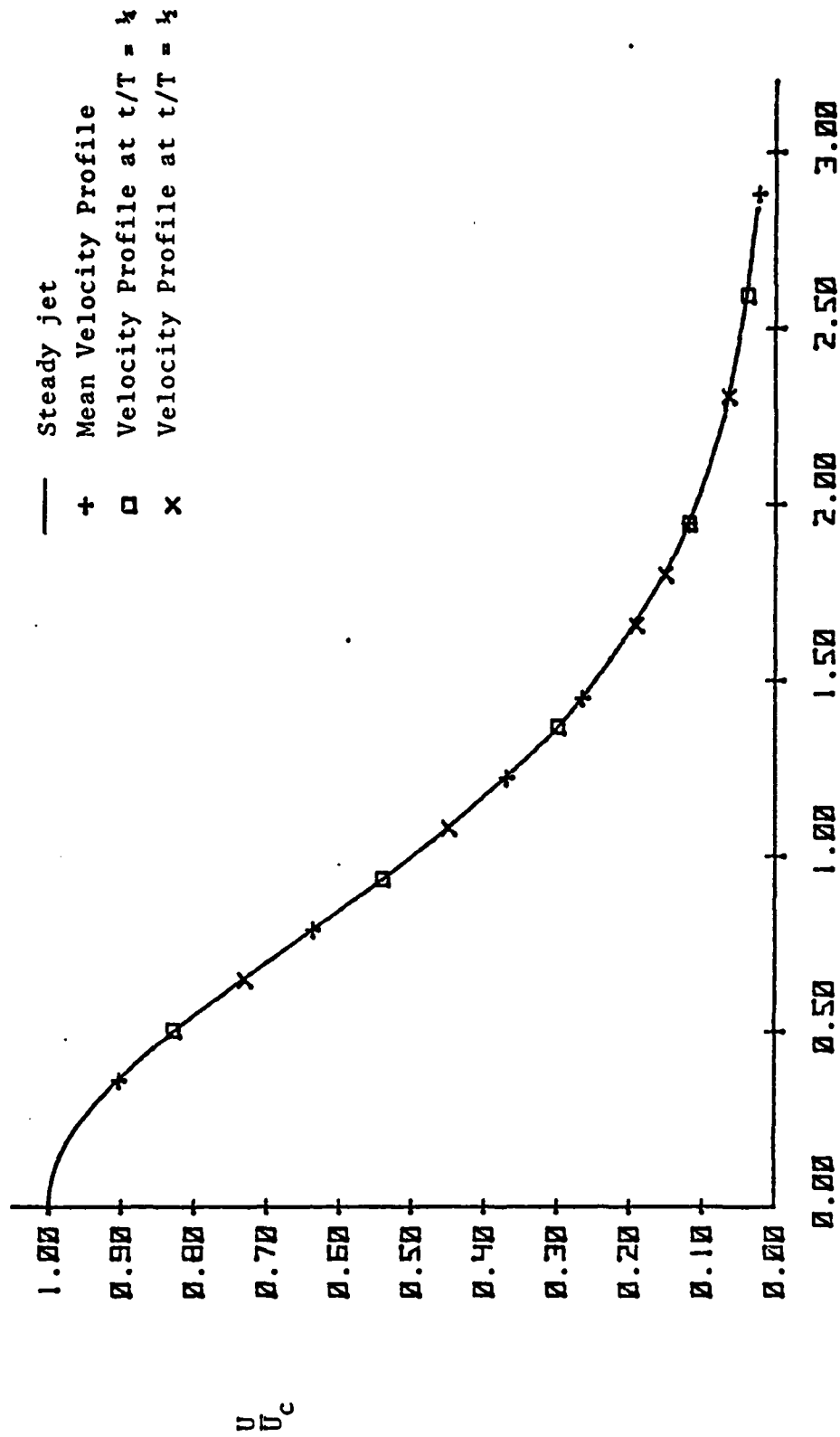


Figure 8(a) Non-dimensional Velocity Distribution for  $\zeta = 40.032$ ,  
 $\omega = 0.000871$ ,  
 $\epsilon = 0.1$

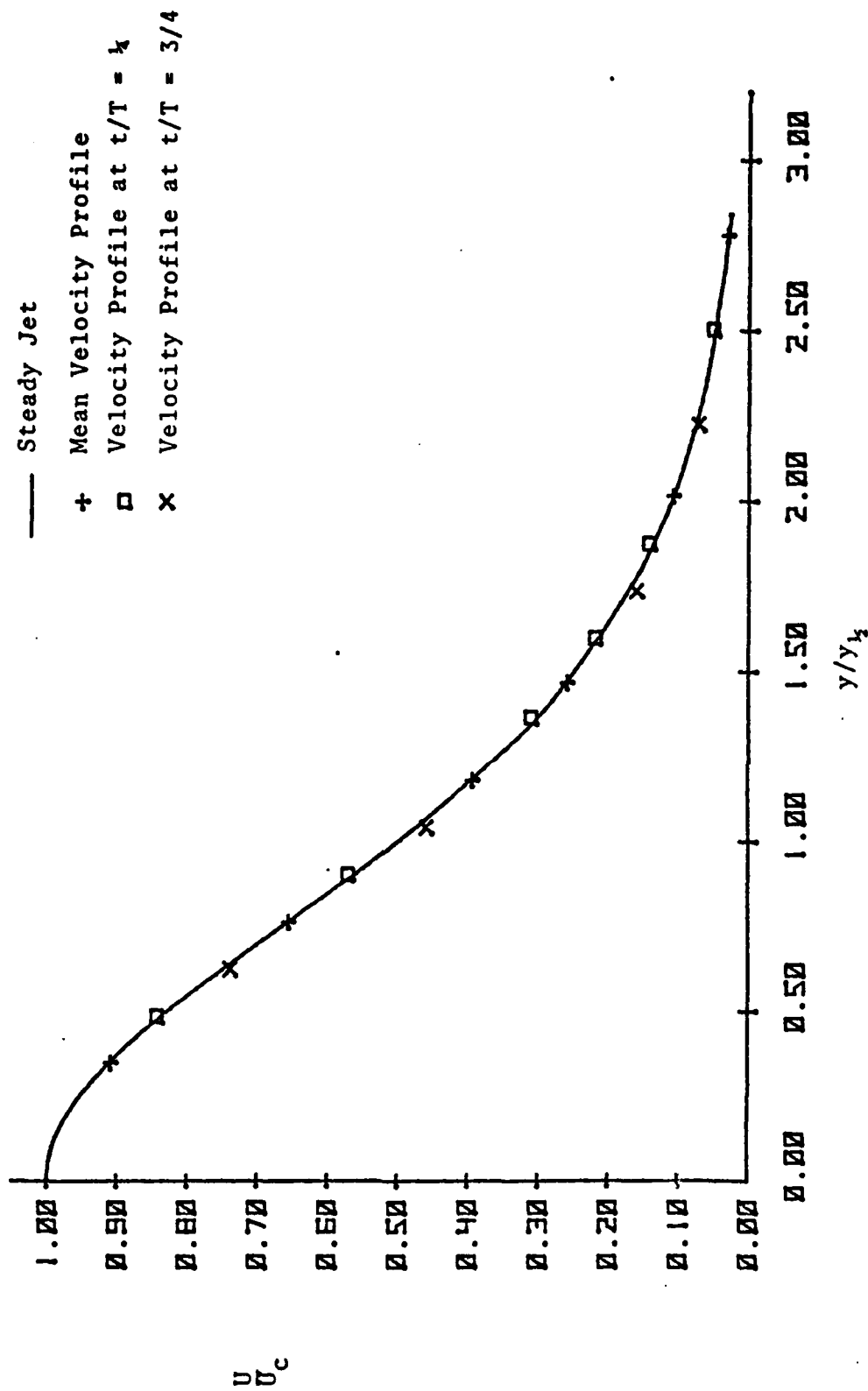


Figure 8(b) Non-dimensional Velocity Distribution for  $\zeta = 40.032$ ,  
 $\omega = 0.00871$   
 $\epsilon = 0.1$

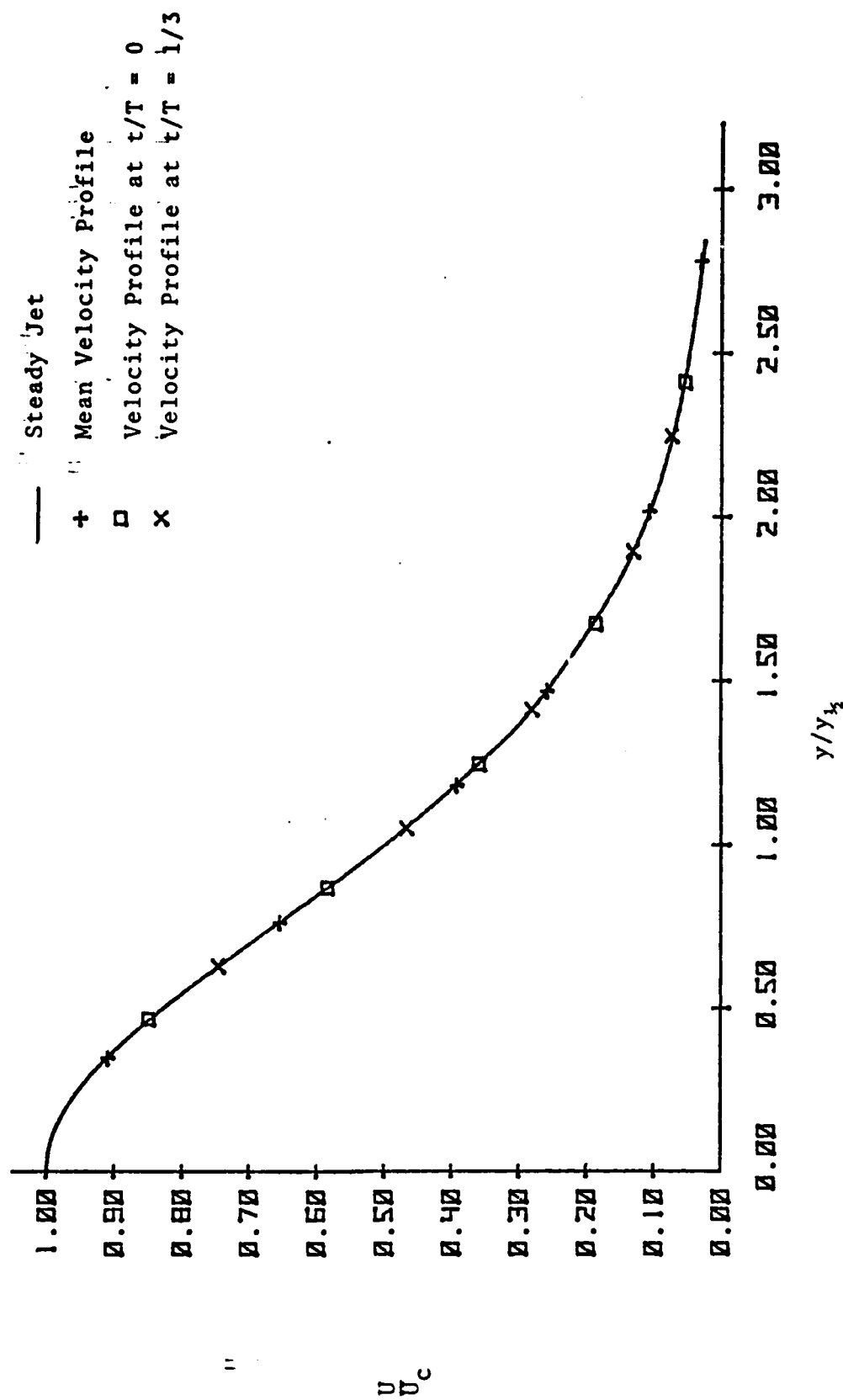


Figure 8(c) Non-dimensional Velocity Distribution for  $\zeta = 40.032$   
 $\omega = 0.0871$   
 $\epsilon = 0.1$

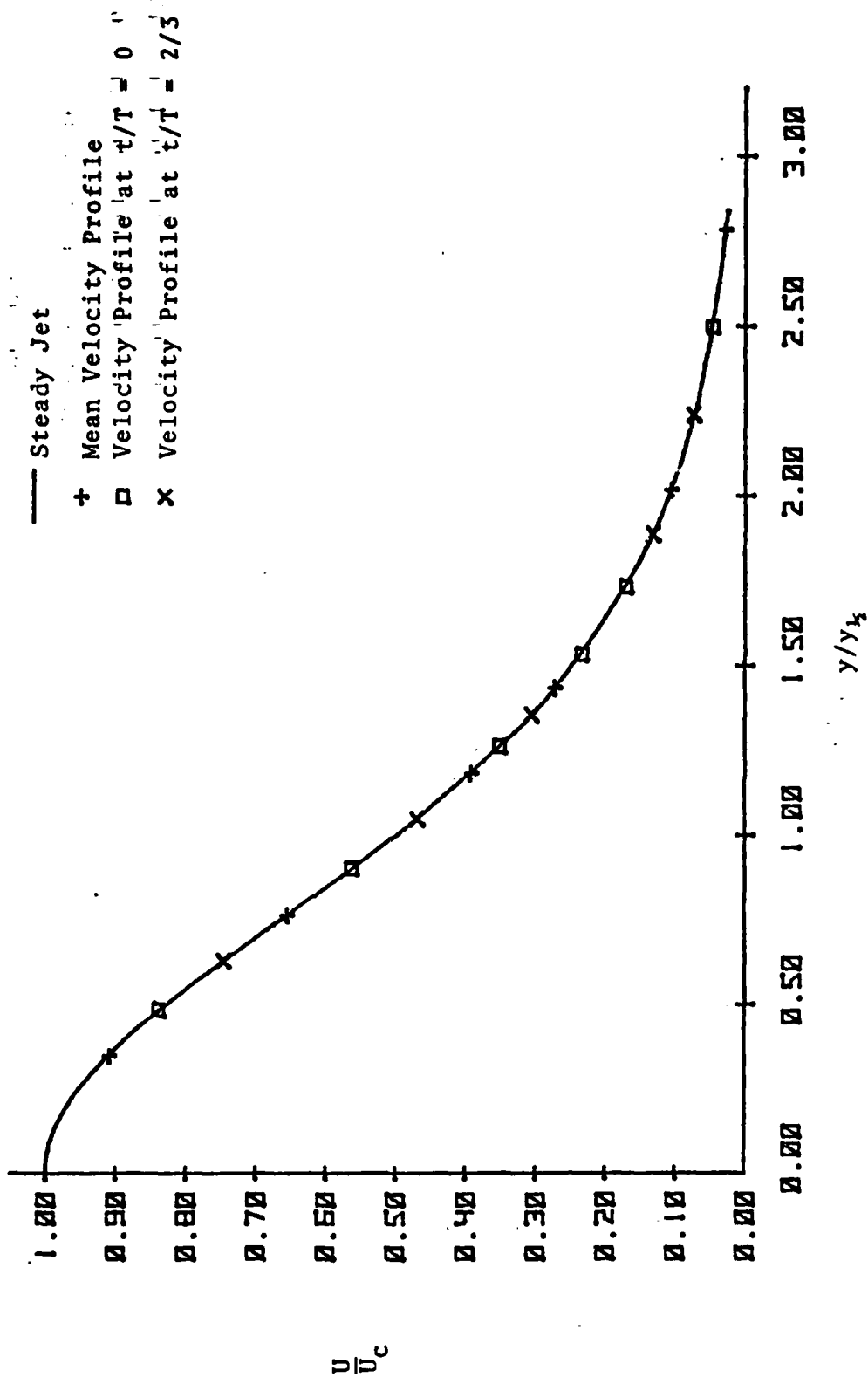


Figure 8(d) Non-dimensional Velocity distribution for  $\zeta = 40.032$   
 $\omega = 0.000871$   
 $\epsilon = 0.15$

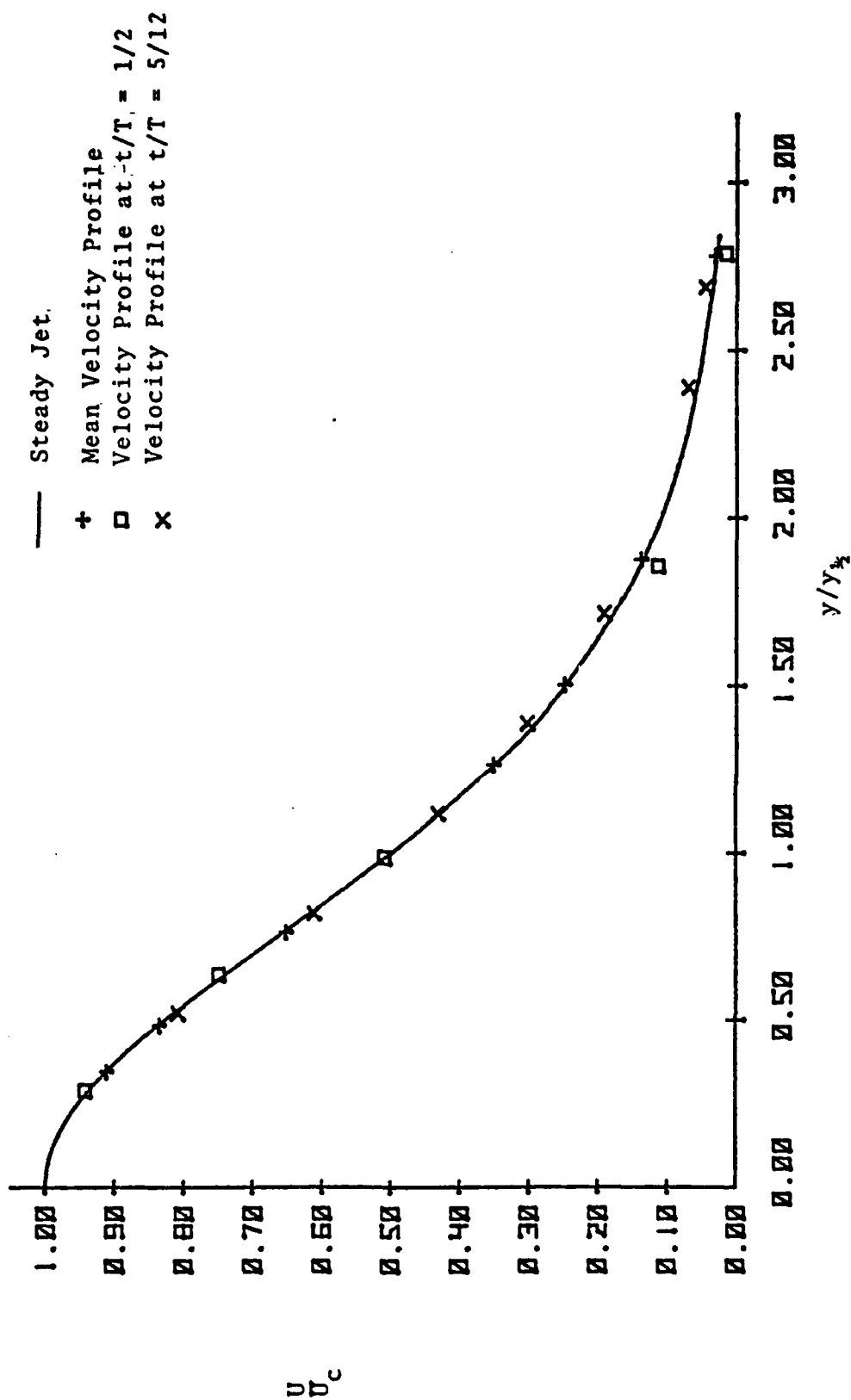


Figure 8(e) Non-dimensional Velocity Distribution for  $\zeta = 40.032$   
 $\omega = 0.00871$   
 $\epsilon = 0.15$

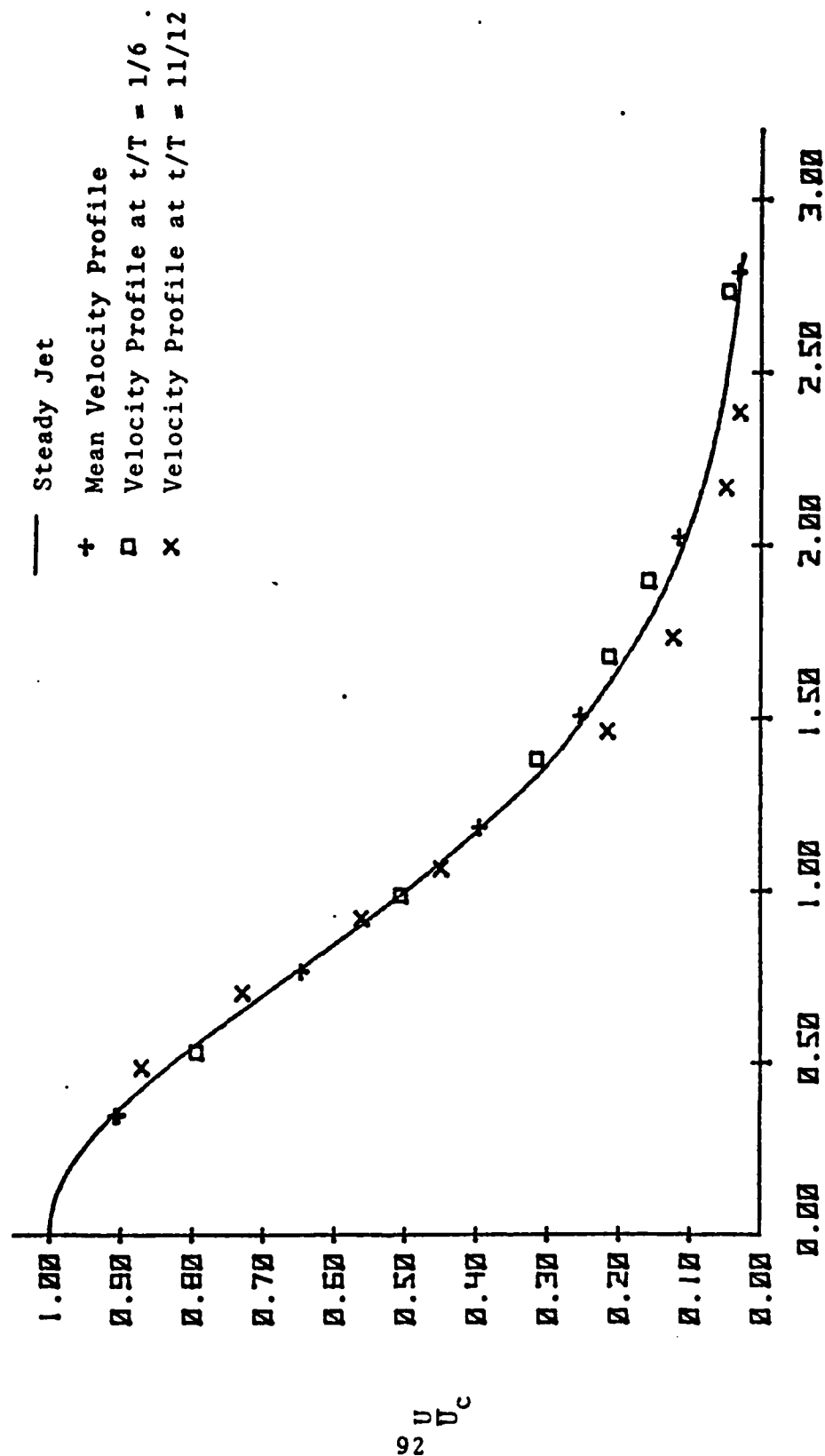


Figure 8 (f) Non-dimensional Velocity Distribution for  $\zeta = 40.032$   
 $\omega = 0.0871$   
 $\epsilon = 0.15$



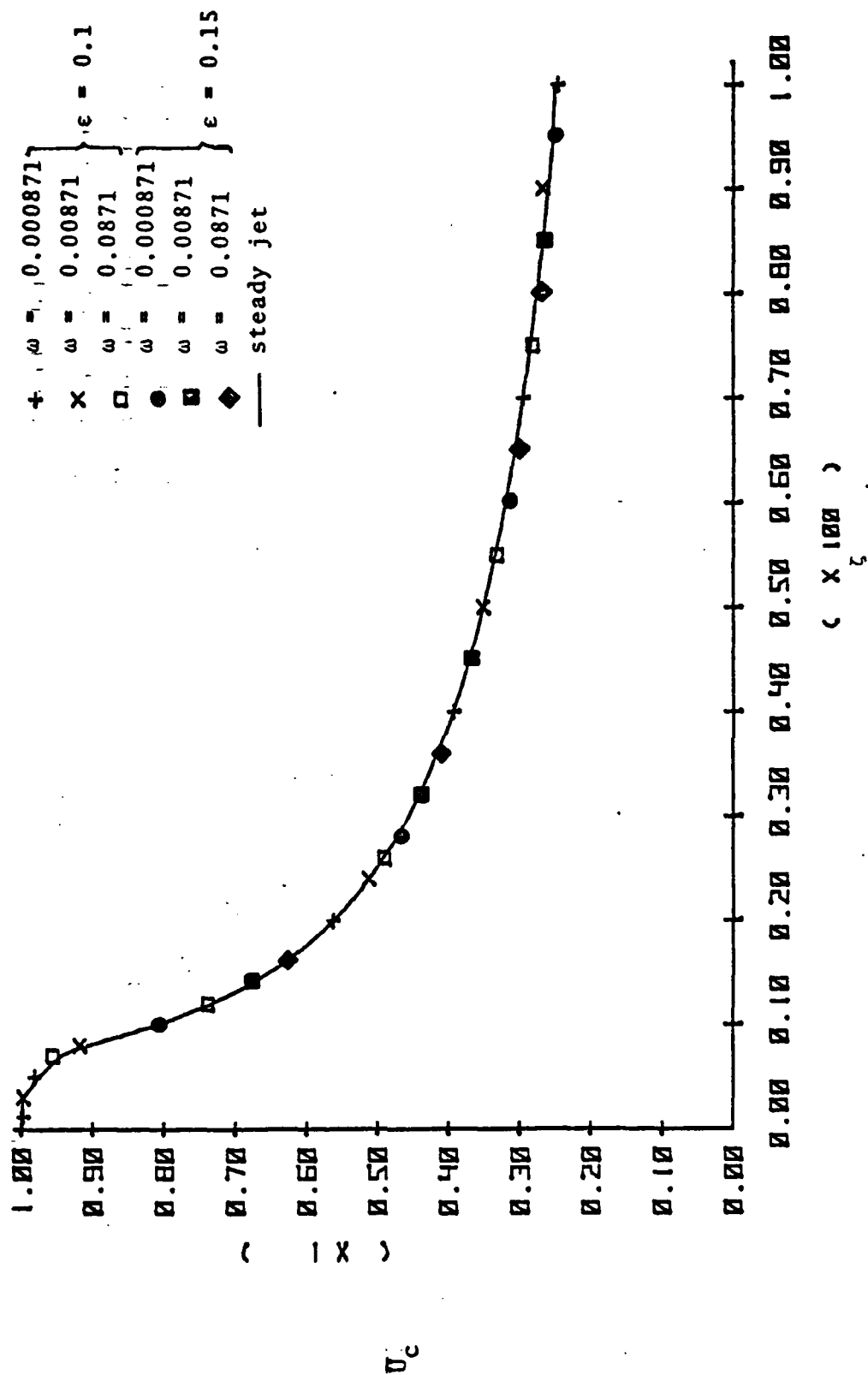


Figure 9 Variation of Mean Centre-Line Velocity with Streamwise Distance

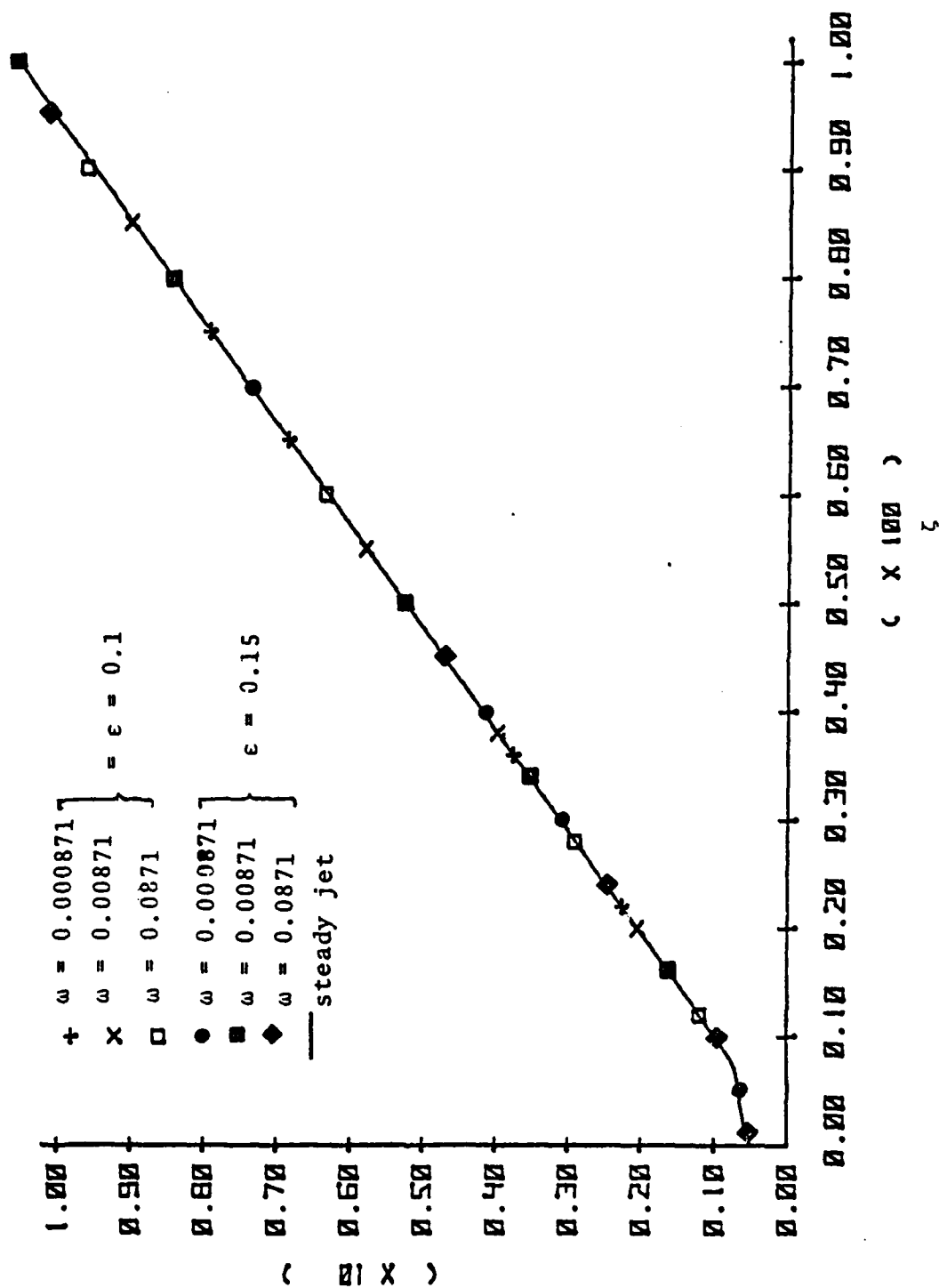


Figure 10 Variation of Mean Jet Half-width Streamwise Distance

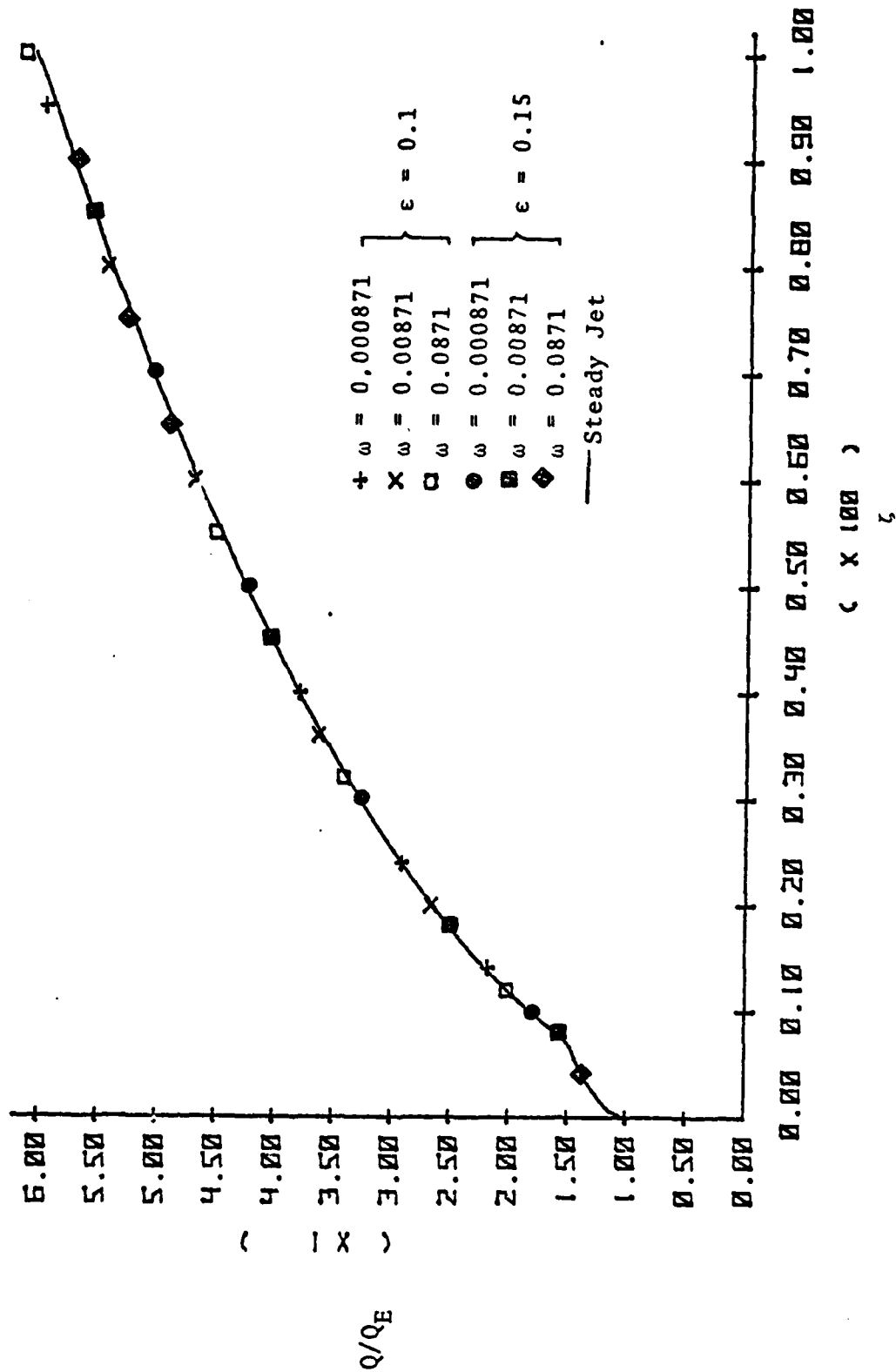


Figure 11 Variation of Non-Dimensional Mass Flow with Streamwise Distance

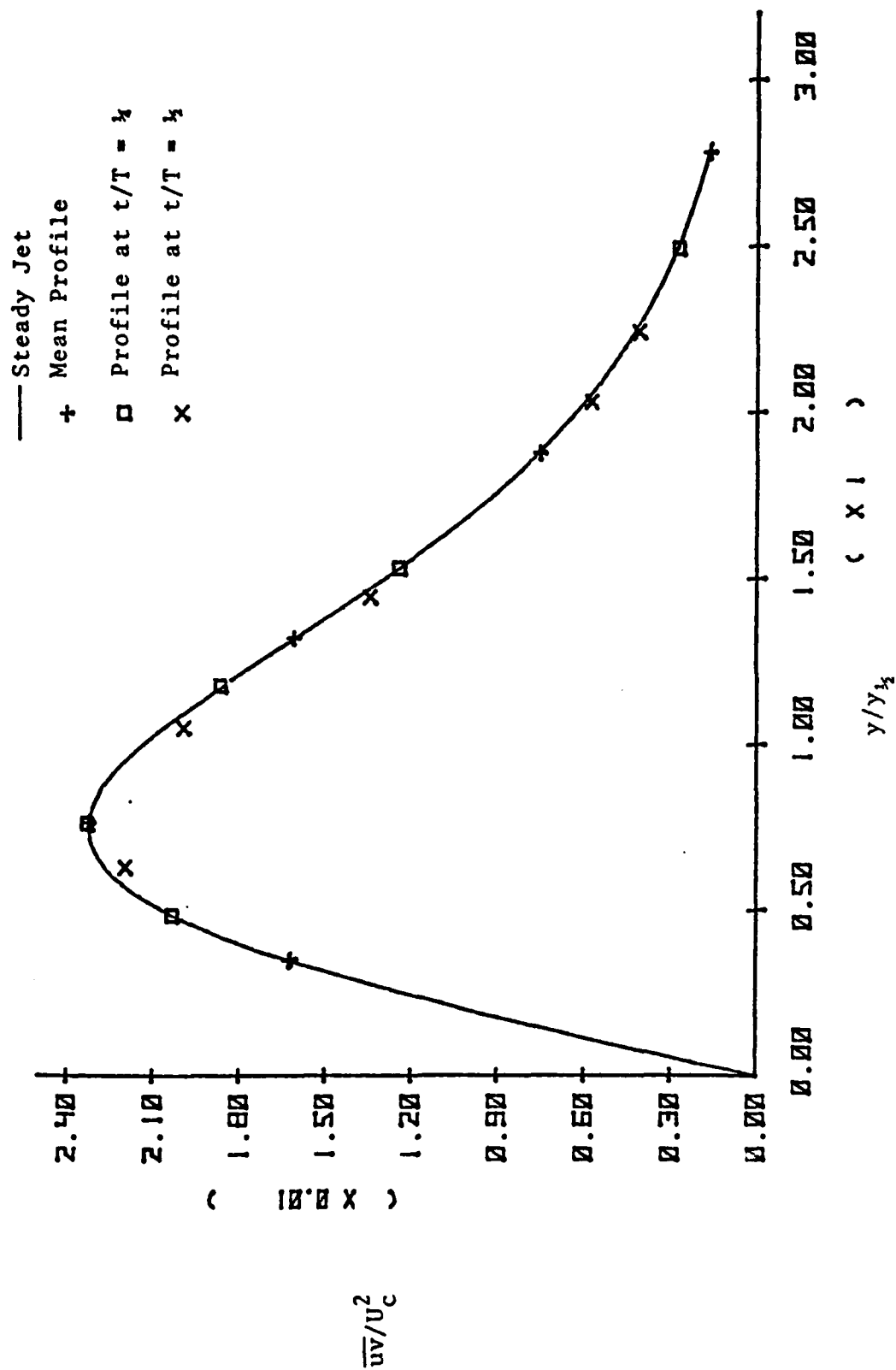


Figure 12(a) Non-Dimensional Shear Stress Profile for  $\zeta = 40.032$ ,  $\omega = 0.000871$ ,  $\epsilon = 0.1$

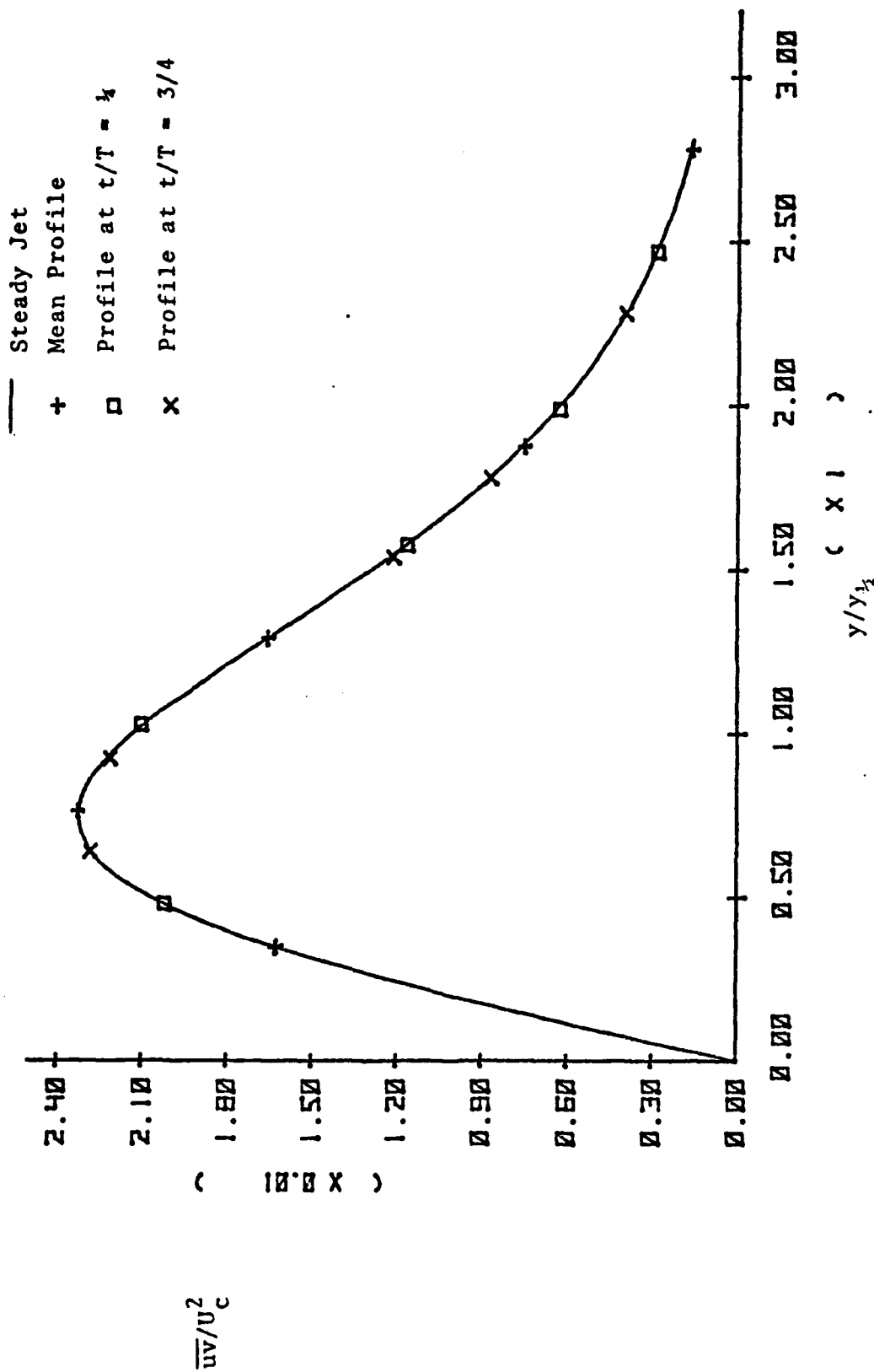


Figure 12(b) Non-dimensional Shear Stress Profile for  $\zeta = 40.032$ ,  $\omega = 0.00871$ ,  $\epsilon = 0.1$

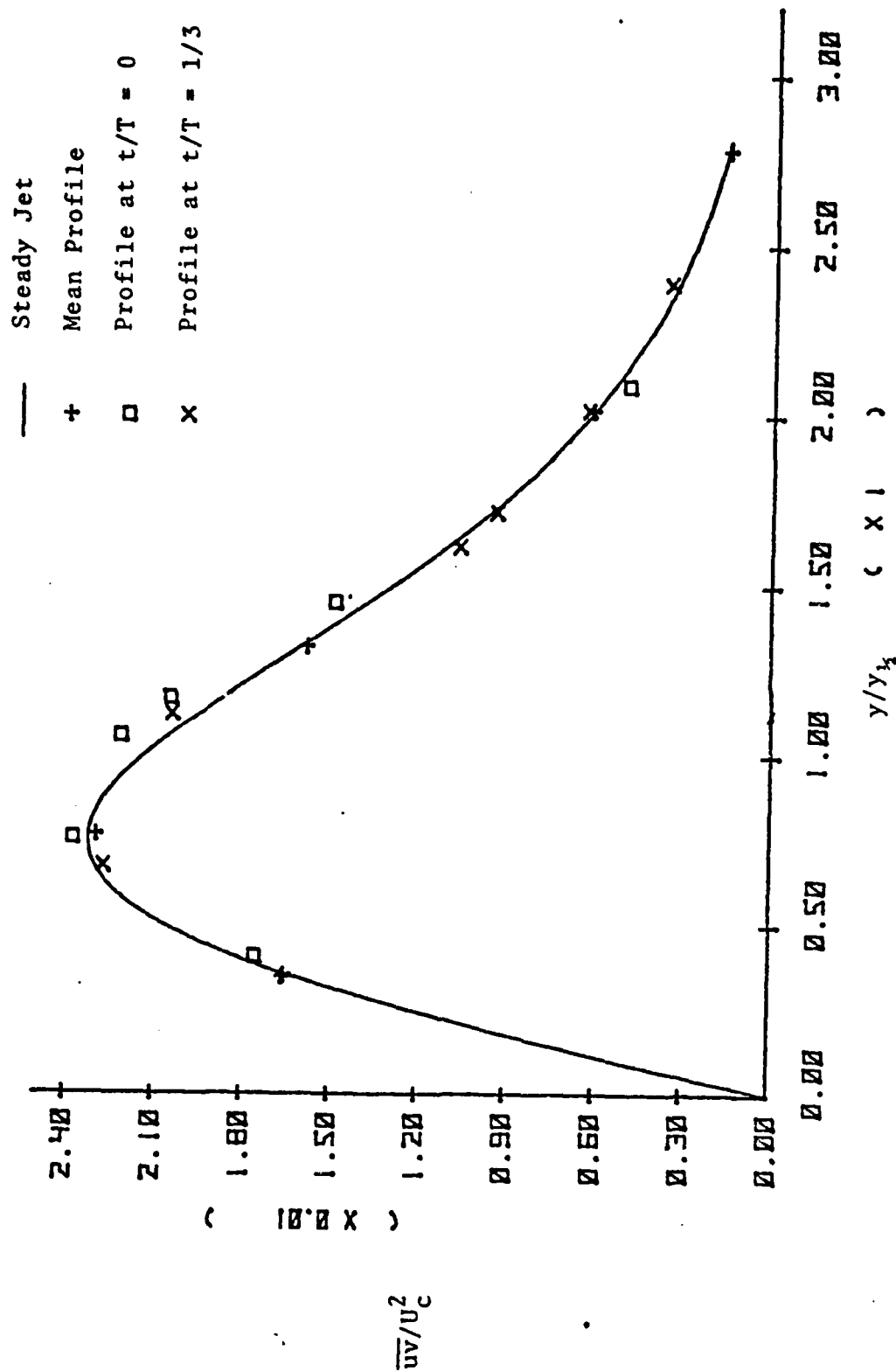


Figure 12(c) Non-dimensional Shear Stress Profile for  $\zeta = 40.032$ ,  $\omega = 0.0871$ ,  $\epsilon = 0.1$

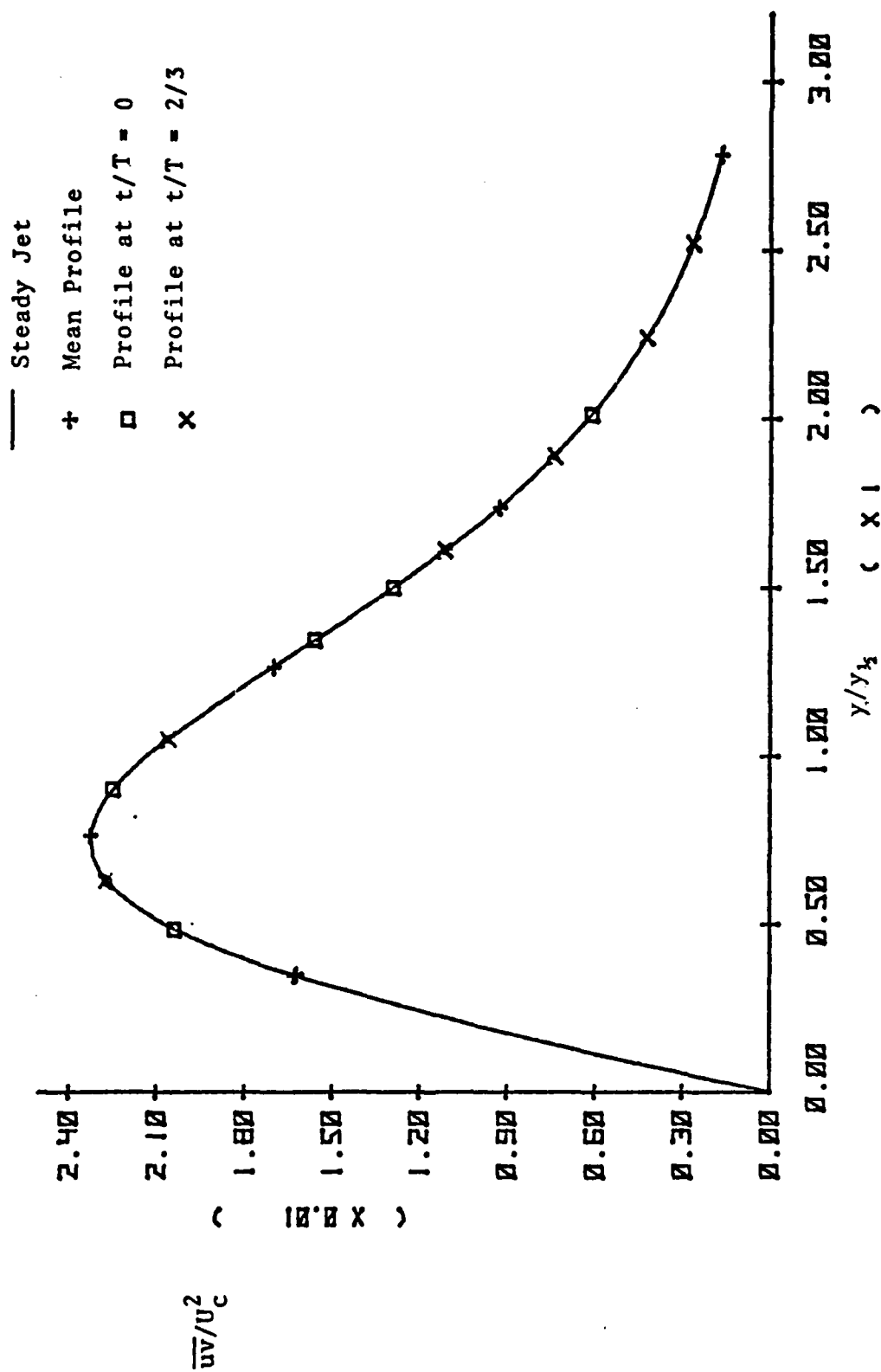


Figure 12(d) Non-Dimensional Shear Stress Profile for  $\zeta = 40.032$ ,  $\omega = 0.000871$ ,  $\epsilon = 0.15$

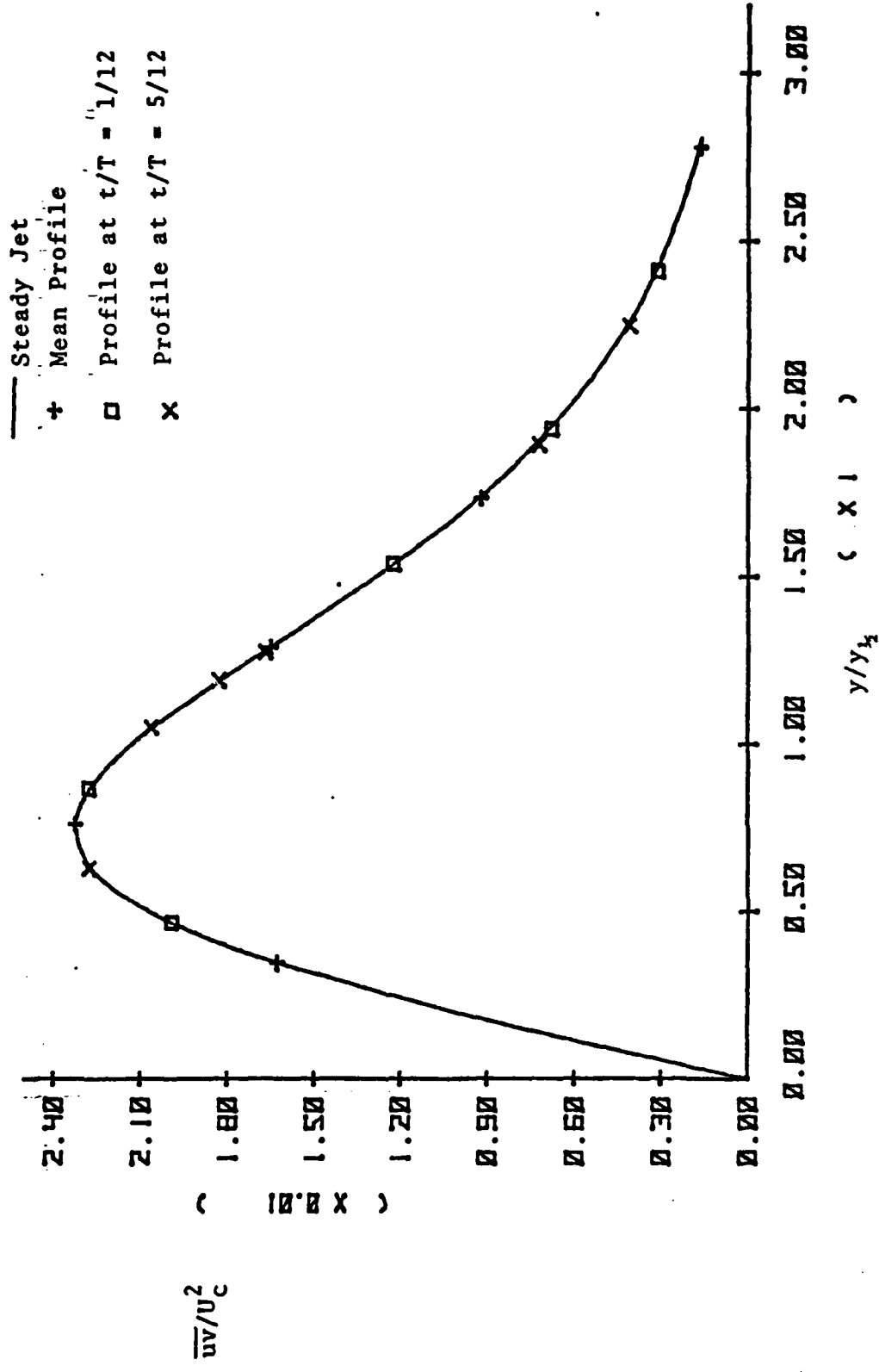


Figure 12(e) Non-Dimensional Shear Stress Profile for  $\zeta = 40.032$ ,  $\omega = 0.00671$ ,  $\epsilon = 0.15$



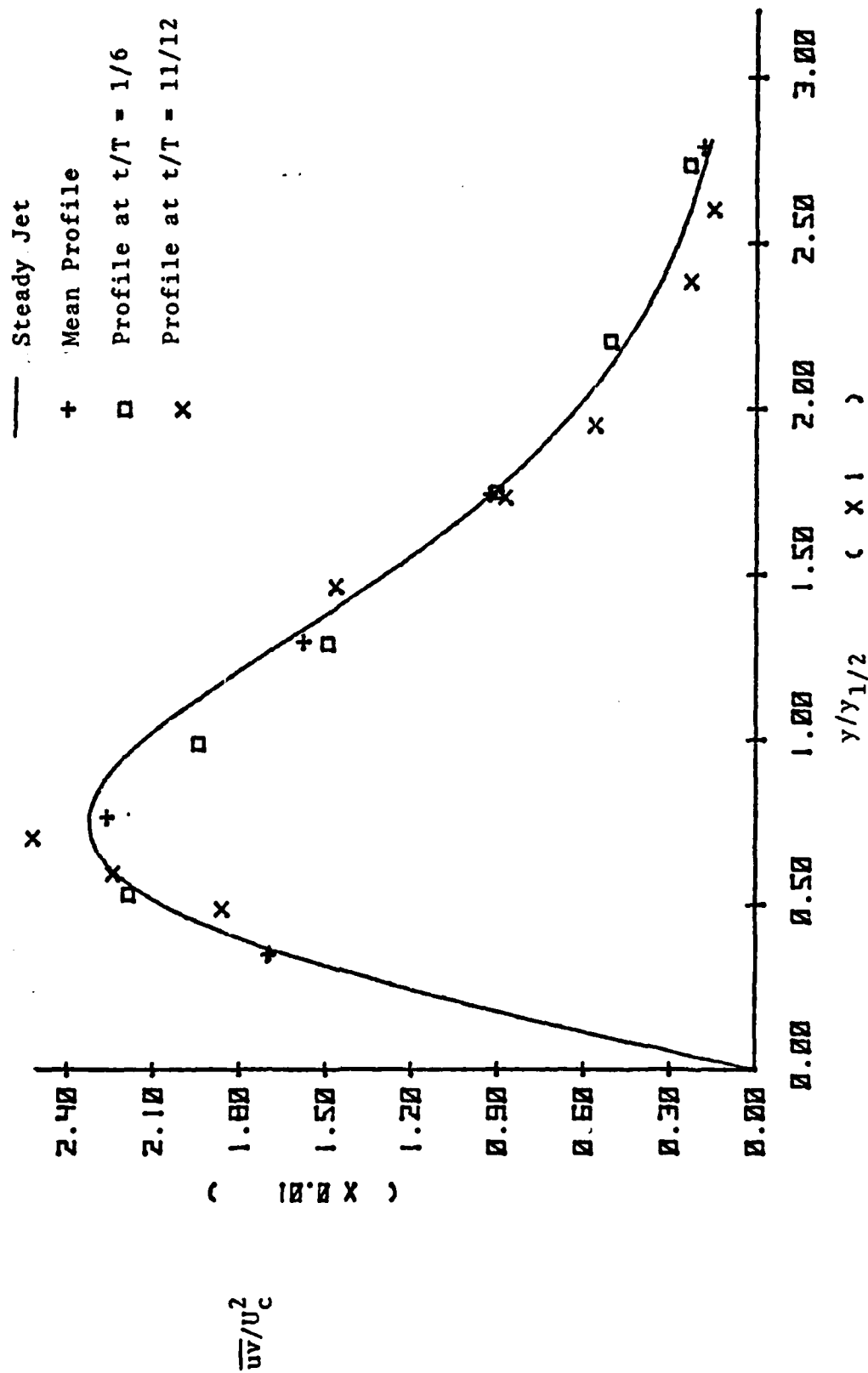


Figure 12(f) Non-Dimensional Shear Stress Profile for  $\zeta = 40.032$ ,  $\omega = 0.0871$ ,  $\epsilon = 0.15$

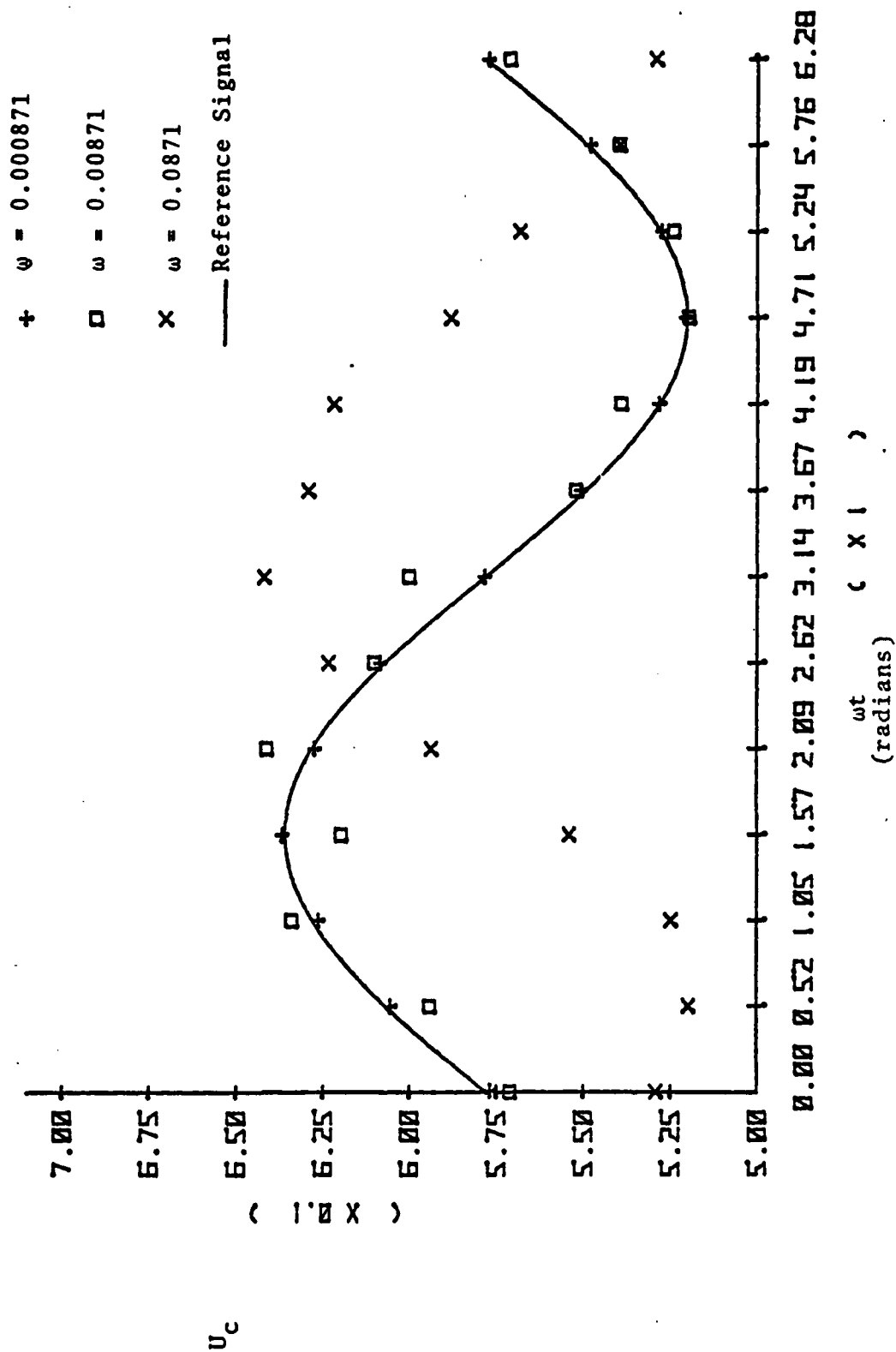


Figure 13(a) Variation of Instantaneous Centre-Line Velocity with Time for  $\zeta = 19.032$   
 $\zeta = 0.1$

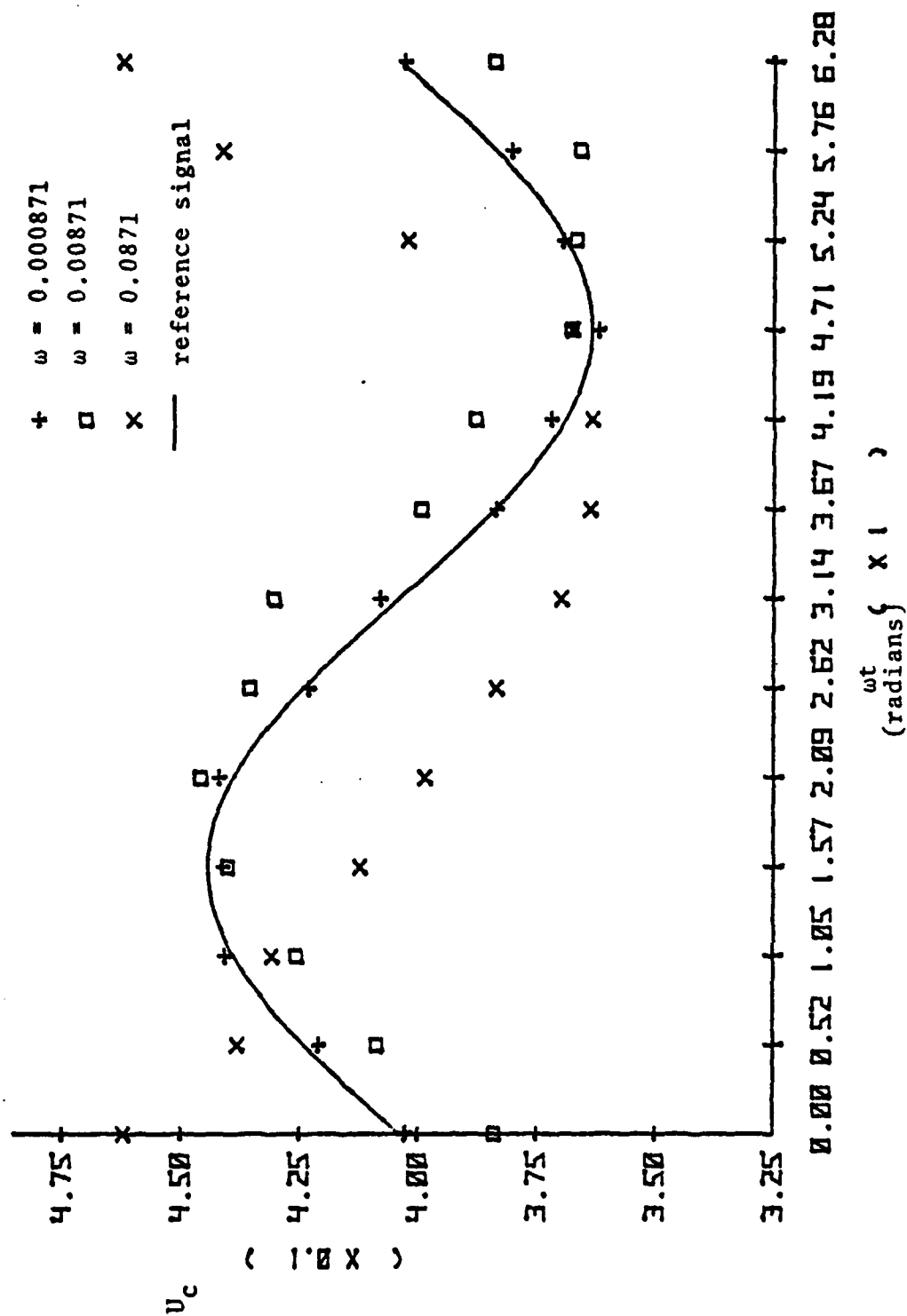


Figure 13(b) Variation of Instantaneous Centre-Line Velocity with Time for  $z = 38.032$   
 $\epsilon = 0.1$

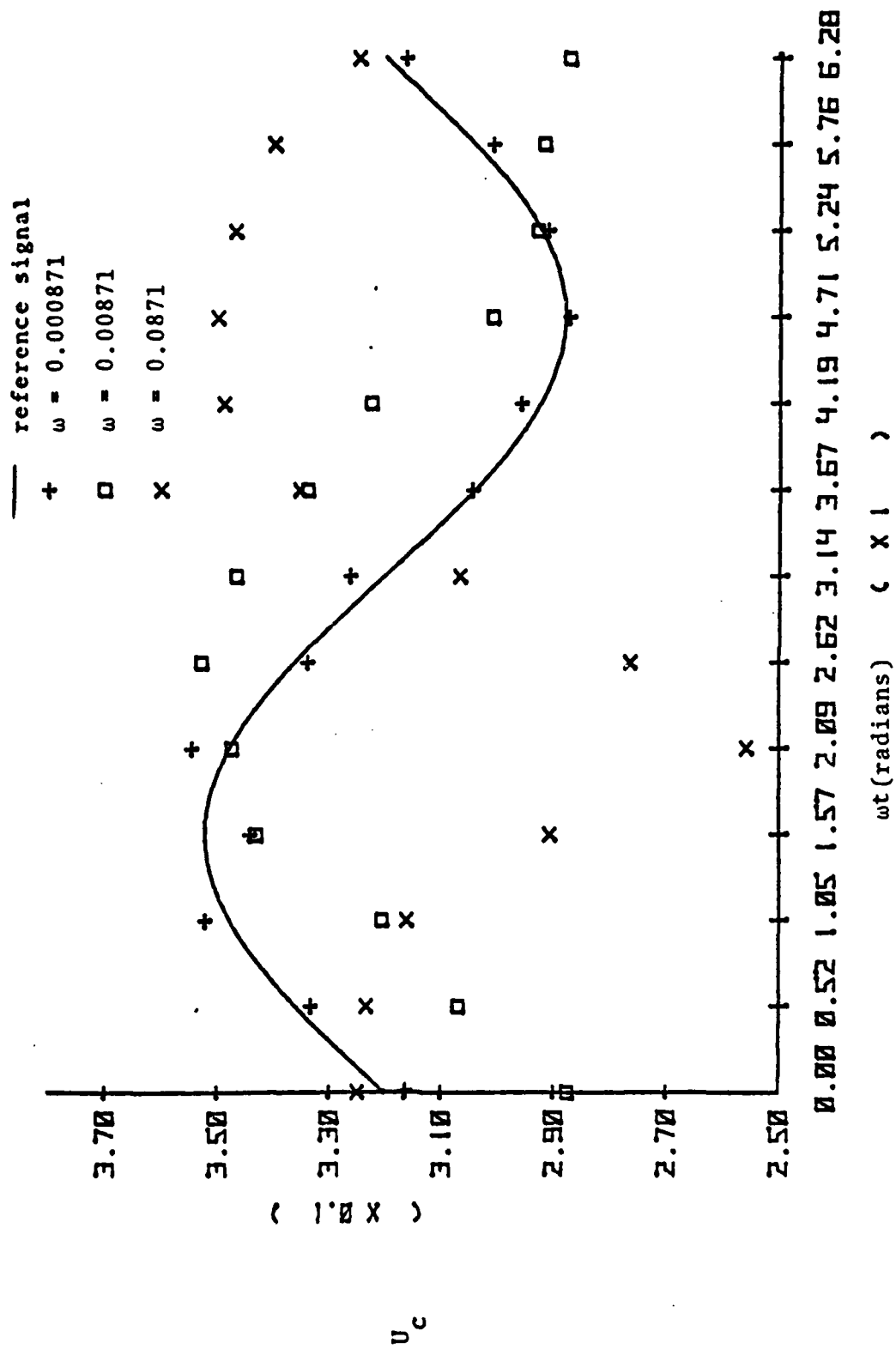


Figure 13(c) Variation of Instantaneous Centre-Line Velocity with Time for  $\zeta = 60.032$   
 $\epsilon = 0.1$

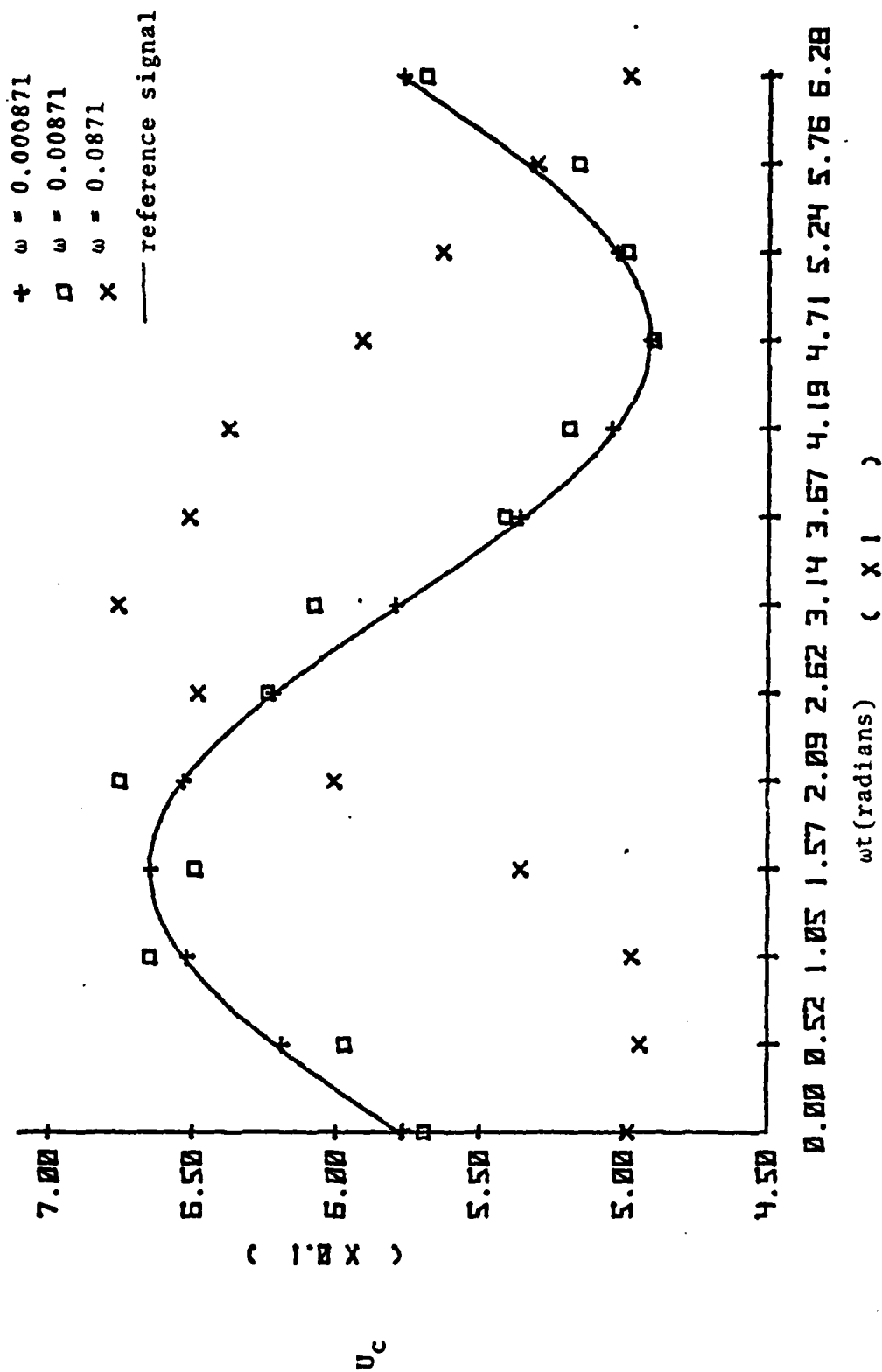


Figure 13(d) Variation of Instantaneous Centre-line Velocity with Time for  $\zeta = 19.032$   
 $\epsilon = 0.15$

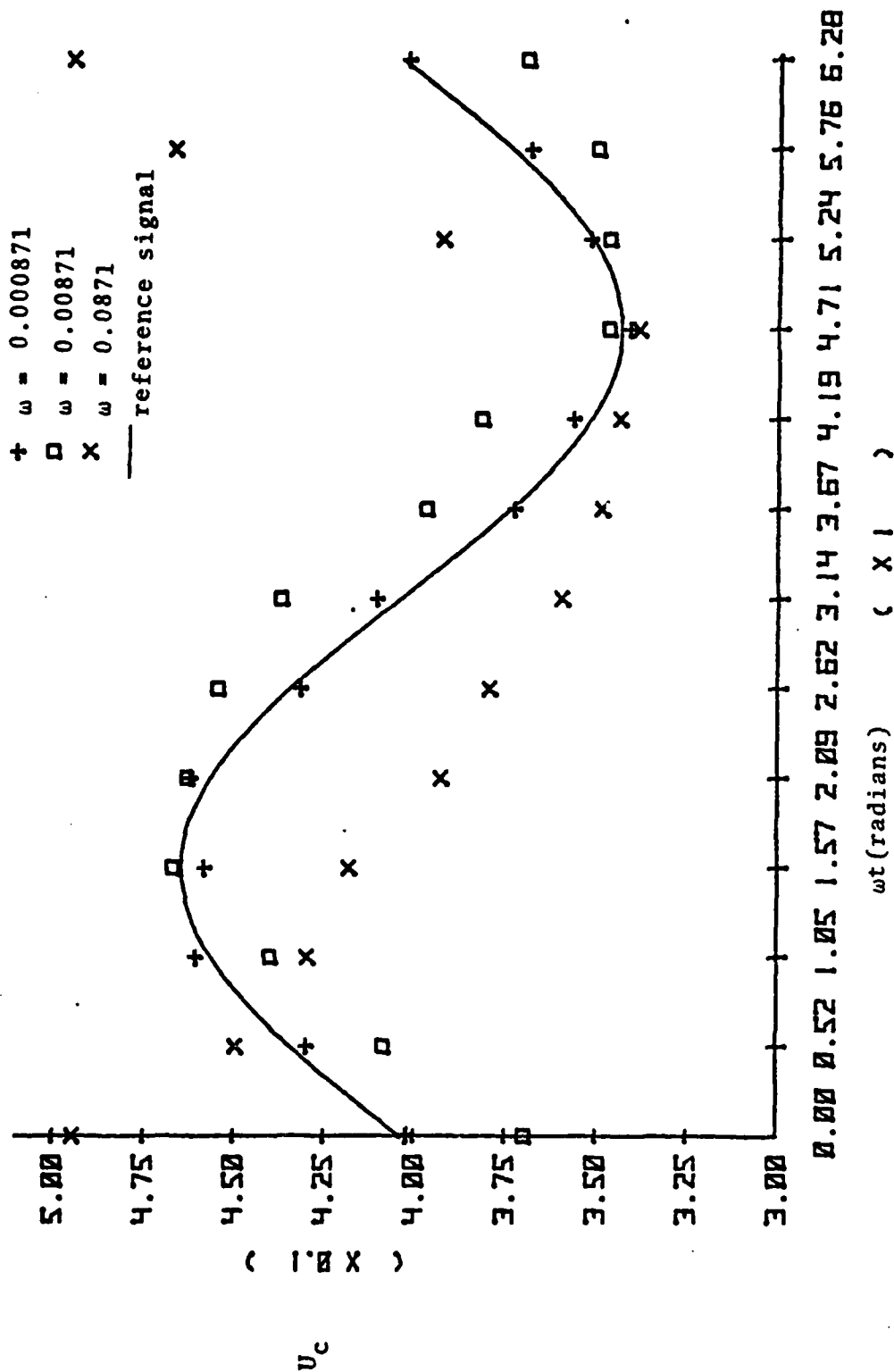


Figure 13(e) Variation of Instantaneous Centre-Line Velocity with Time for  $\zeta = 38.032$   
 $\epsilon = 0.15$

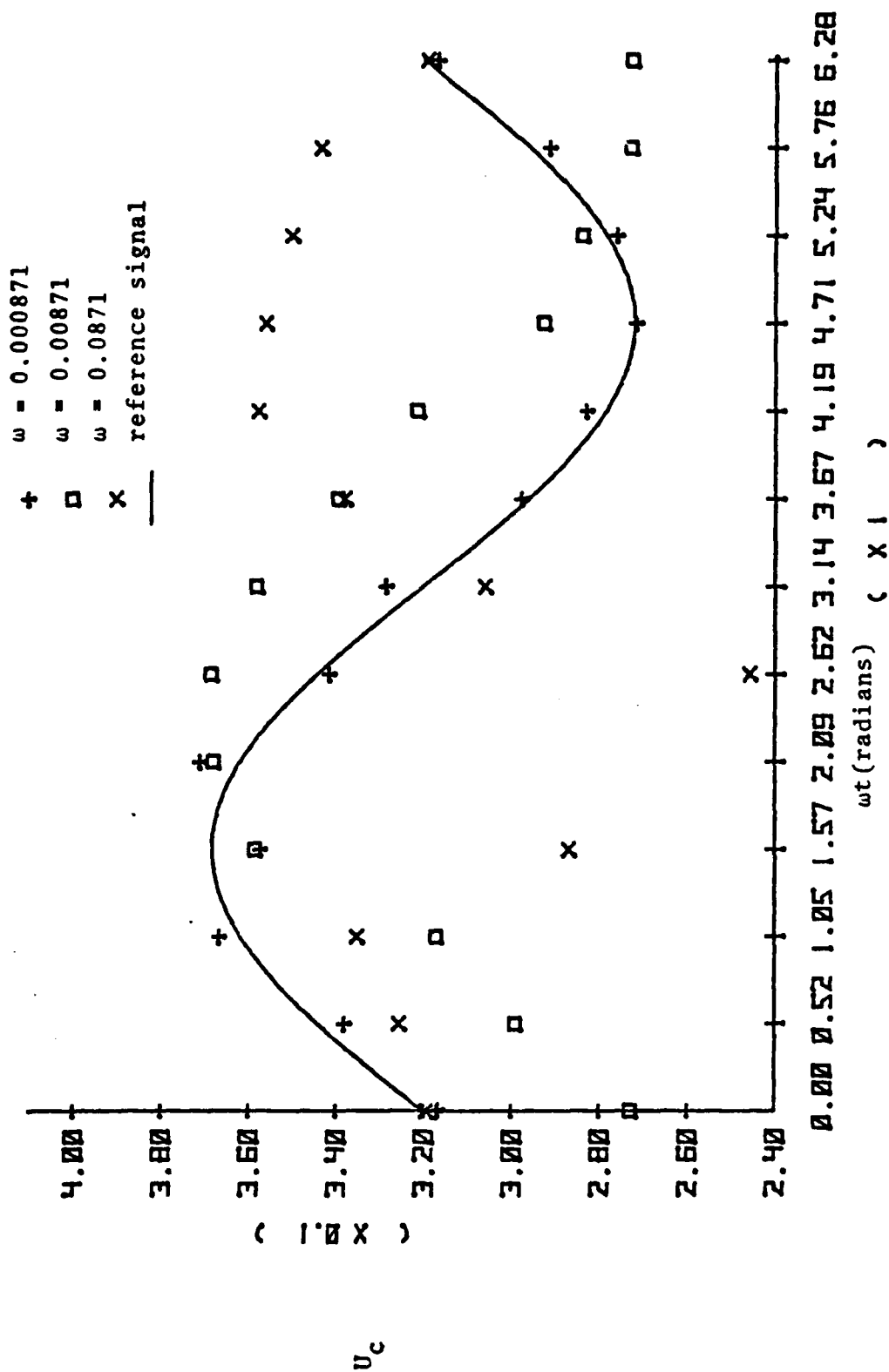


Figure 13(f) Variation of Instantaneous Centre-Line Velocity with time For  $\zeta = 60.032$   
 $\epsilon = 0.15$

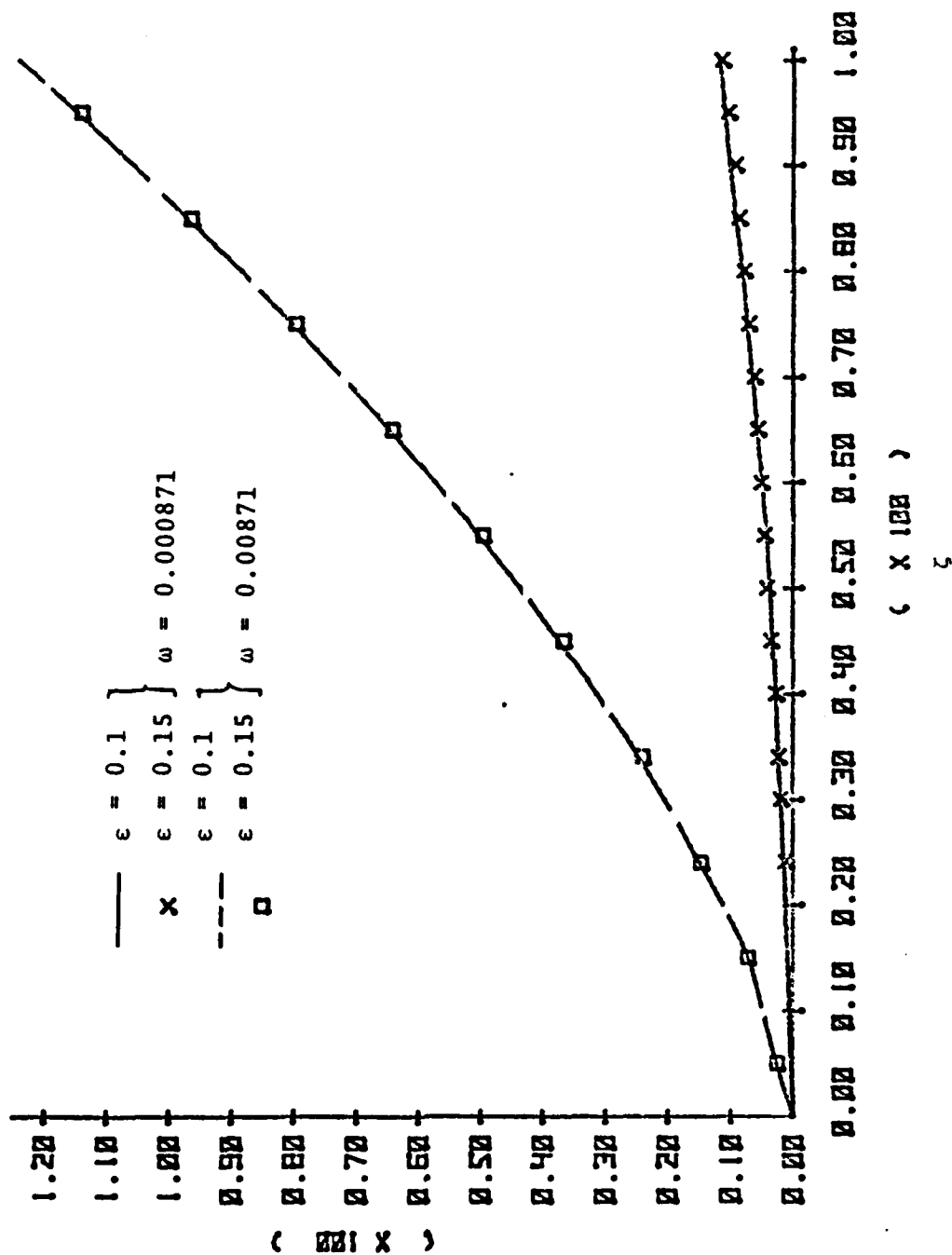


Figure 14(a) Variation of Phase Angle with Streamwise Distance



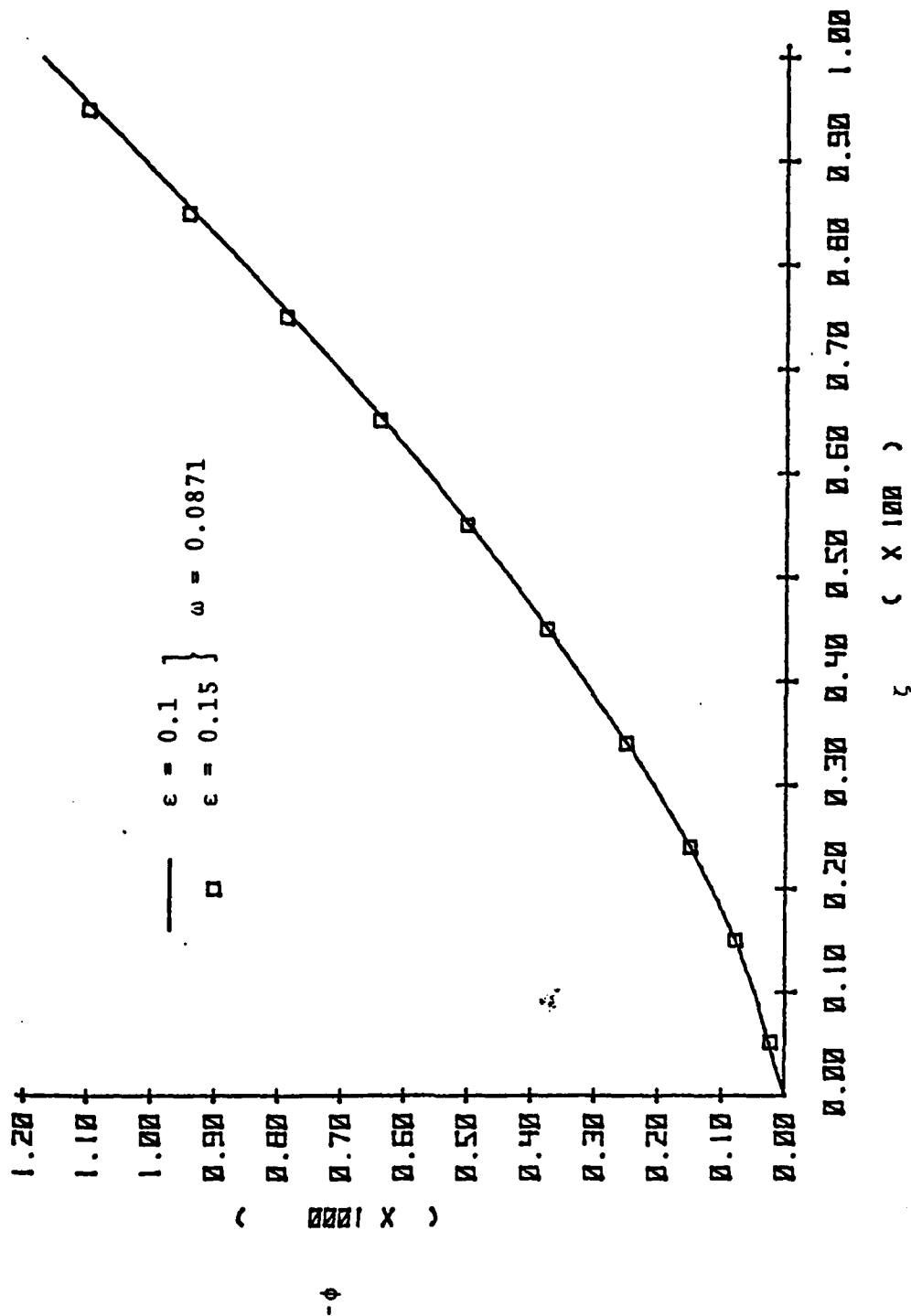


Figure 14(b) Variation of Phase Angle with Streamwise Distance

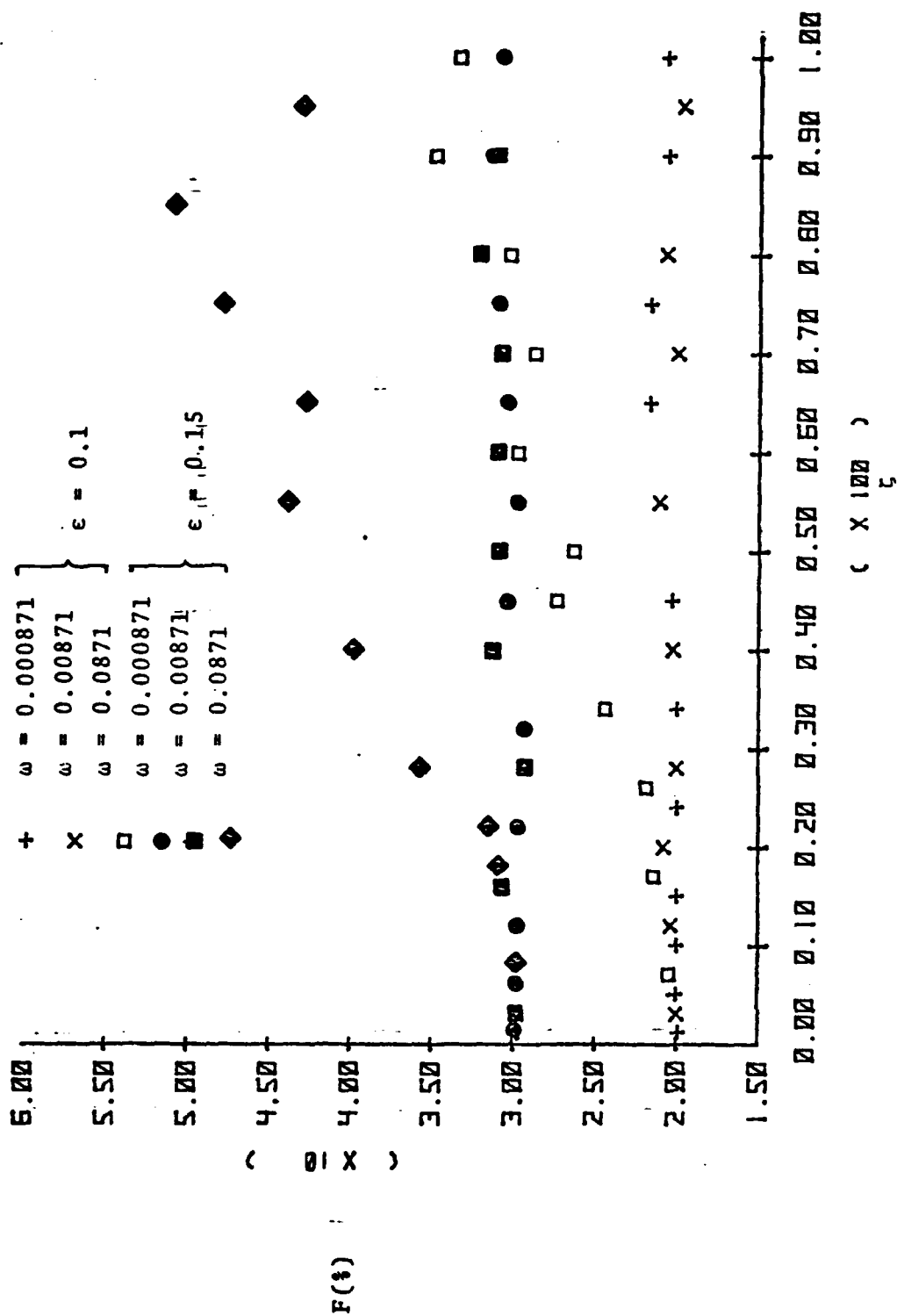


Figure 15 Variation of Peak-to-Peak Oscillation of Centre-Line Velocity with Streamwise Distance

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